

School of Industrial and Information Engineering
Course 096125 (095857)
Introduction to Green and Sustainable Chemistry

 POLITECNICO DI MILANO

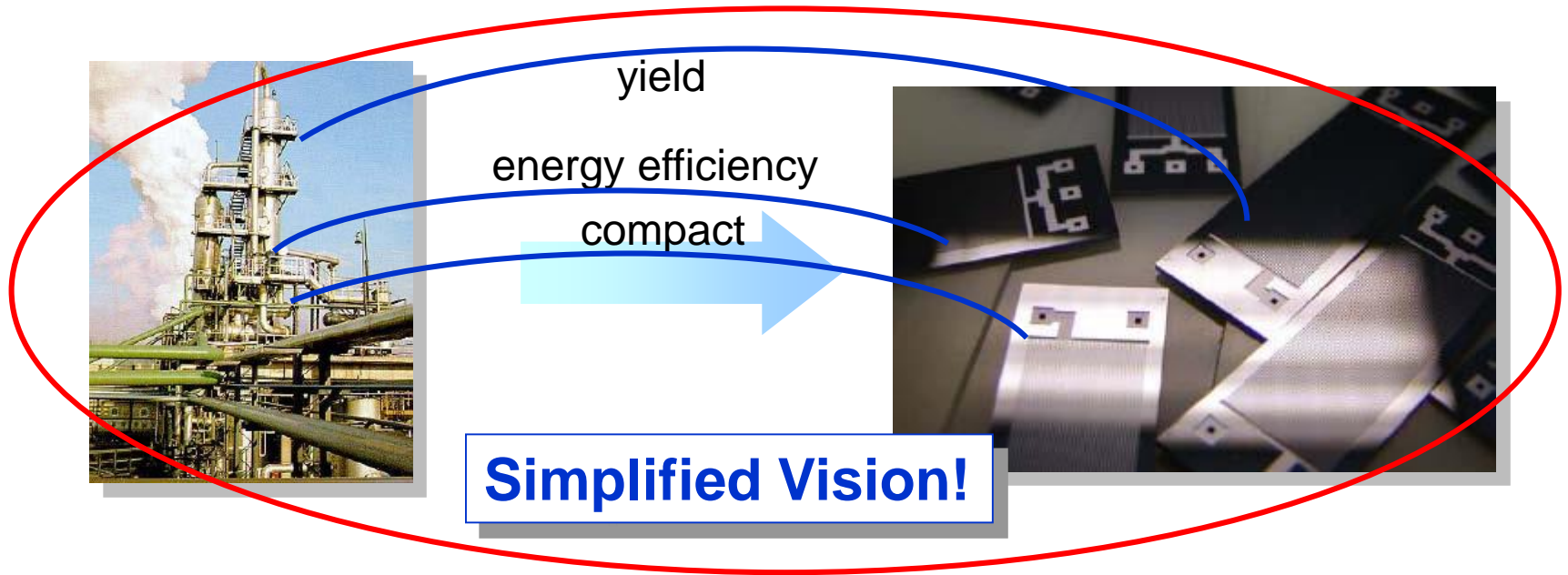


Microchemical and Microphysical Systems.

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Dipartimento CMIC “Giulio Natta”

<https://iscamapweb.chem.polimi.it/citterio/it/education/course-topics/>

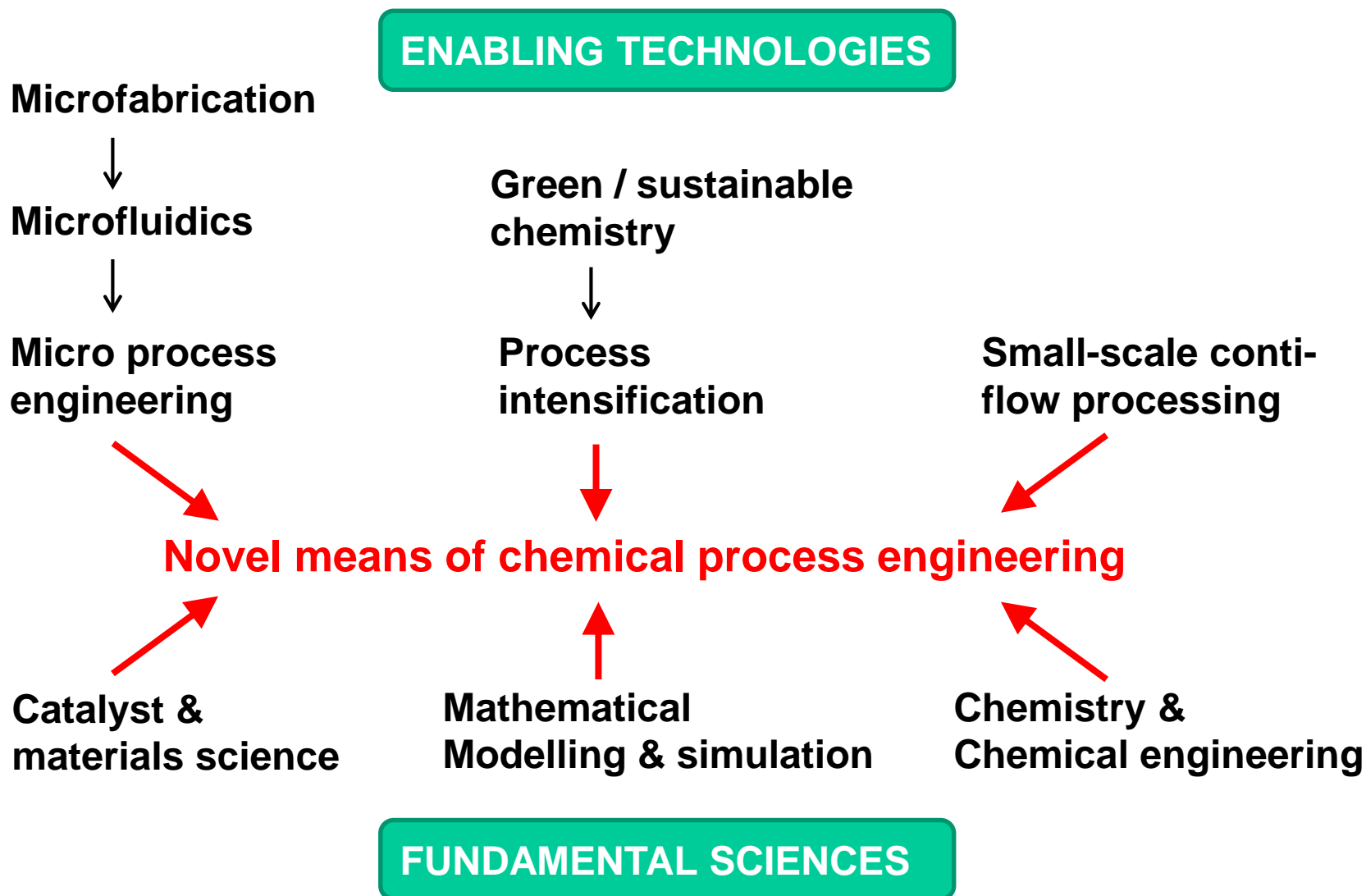
Micro-chemical Systems and Processes: Opportunity and Limits.



Miniature reaction and other unit operations, show *specific advantages* over conventional chemical systems.

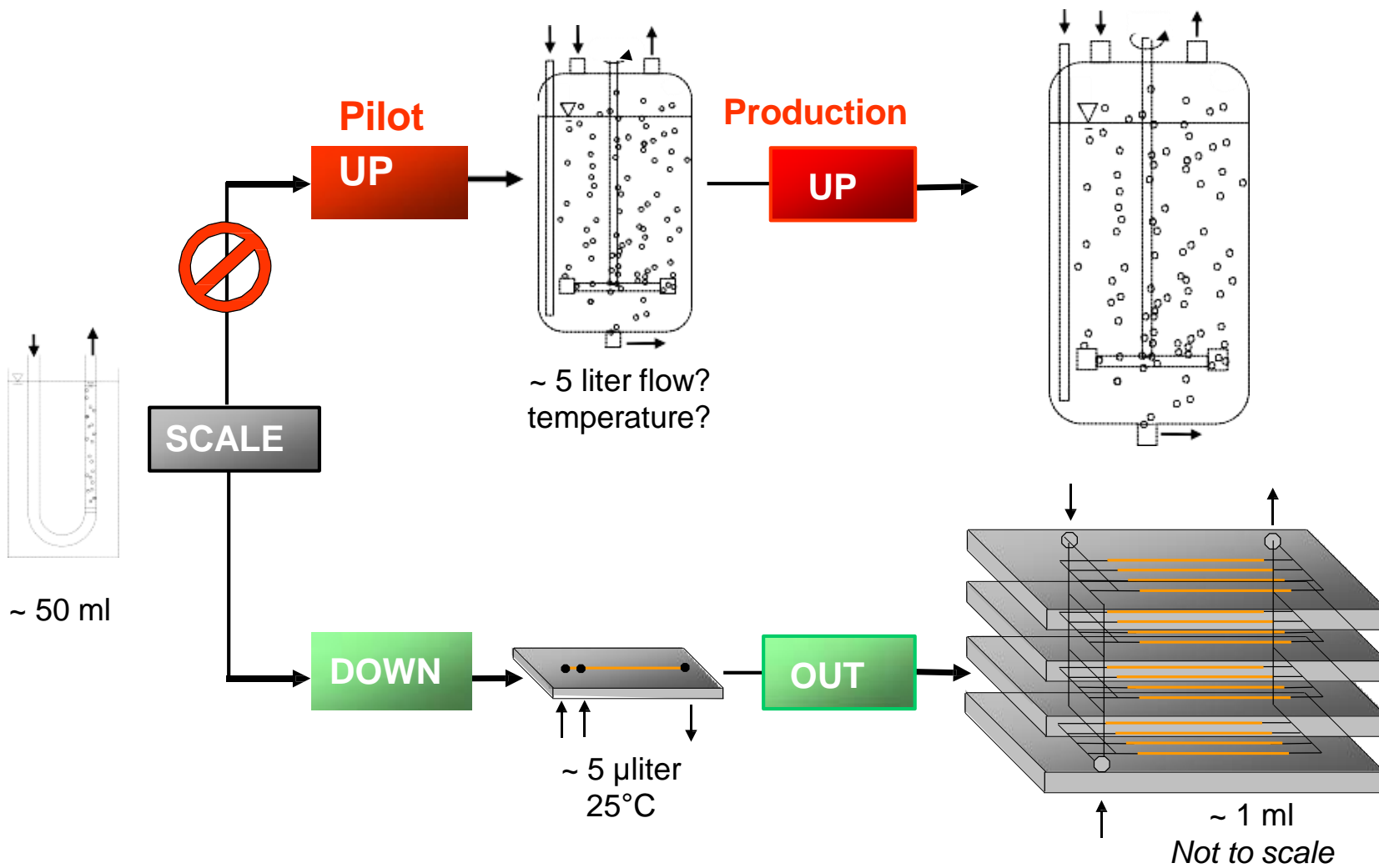


Modern Trends in Chemistry & Chemical Engineering Crossing Discipline Boundaries.





Microchemical Systems – Scale Down and Out.



MIT



Fine-Chemical Microreactors Production Plant.

IMM Plant in NATURE
Nature 442, 27 July 2006



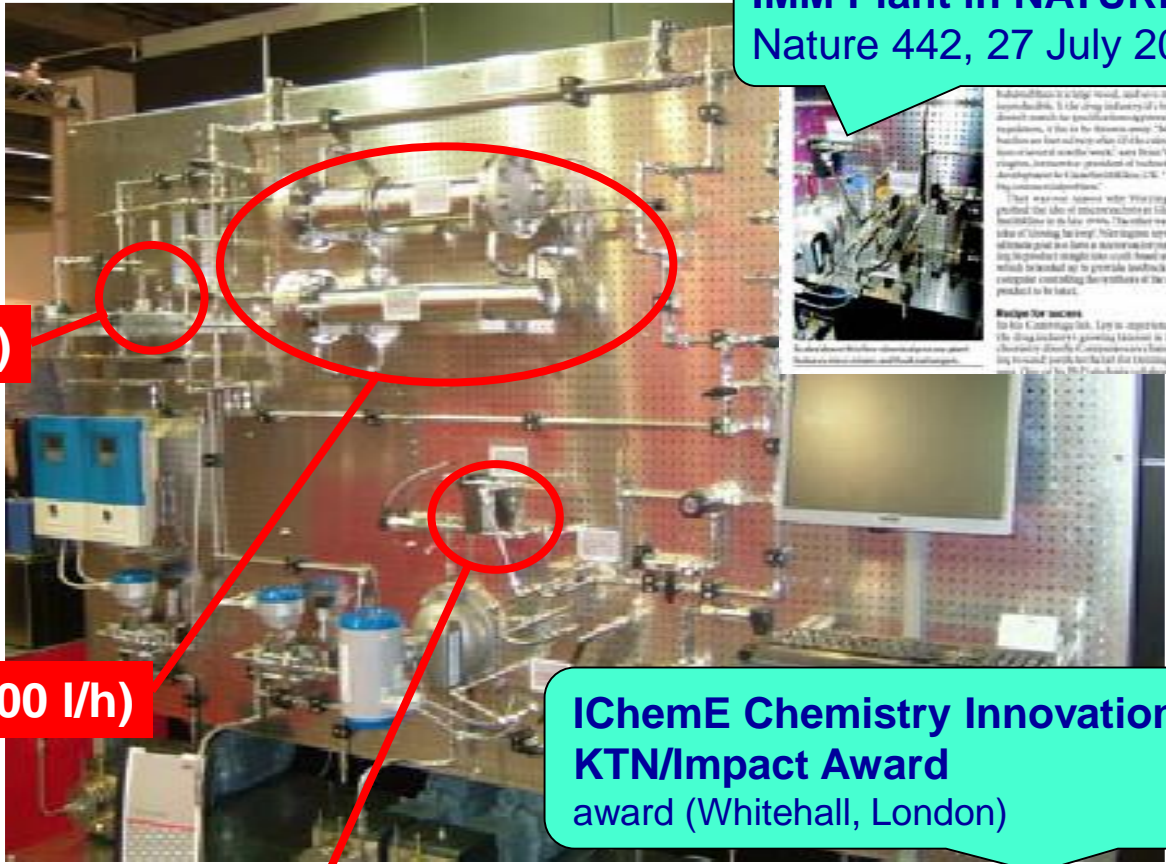
Micromixer (1000 l/h)



Microtube reactor (100 l/h)



Micro heat exchanger (100 l/h)



**IChemE Chemistry Innovation
KTN/Impact Award**
award (Whitehall, London)

**Fine-chemical plant with 10 microstructured
production devices: launch at ACHEMA, May 15, 2006**



Chemical Process Miniaturization.

“Miniature version of the regular thing.”

- Same functionality per volume as macro
- Miniature size is distinguishing factor
- Portability often important
- Often highly integrated
- Microscale platforms for nanoscale structures/materials.
- New technologies and electronic controls.
- Application of microfluids.



What is Microfluidics?

Microfluidics enables precise control, manipulation and analysis of fluids in the microliter to picoliter range. Microfluidic devices are fabricated using techniques developed in the semiconductor industry and are often referred to as microfluidic chips. Today the main application areas for microfluidics include:

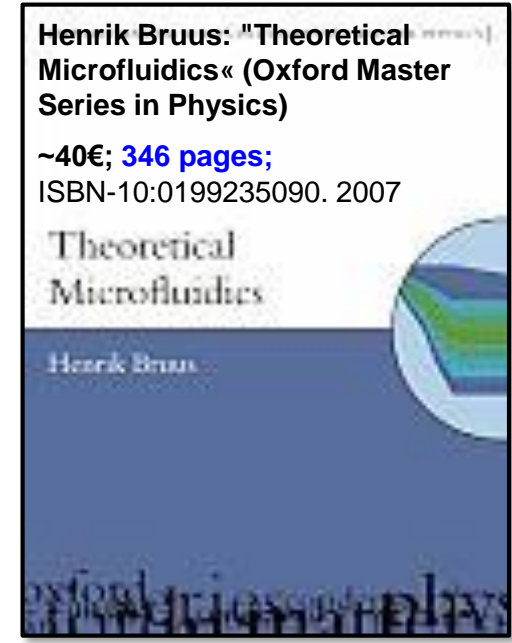
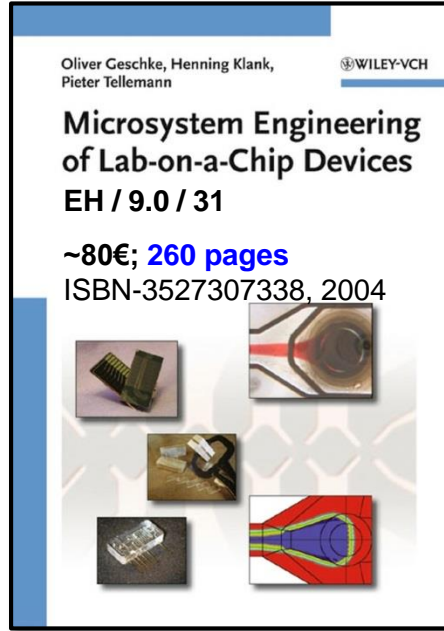
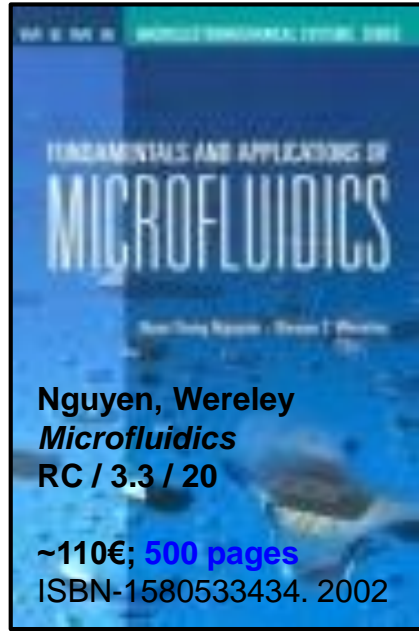
- Research and development chemistry
- DNA analysis and genomics
- Microreactors
- Cell based systems
- Microarrays
- Clinical diagnostics
- Liquid chromatography
- Bio-defence sensors

The benefits of using microfluidic devices for laboratory applications include:

- Reduction in sample volume and reagent usage
- Improved resolution of separations
- Ability to run reaction and analysis processes faster
- Ability to run processes in parallel
- Improved control of mixing and heating of fluids
- Rapid mass transfer as a result of high surface area to volume ratios
- Improved integration of process steps, for example reactions and separations
- Development of new and improved detection methods
- Simpler and cheaper disposable devices
- Access to a wide range of fluidic geometries.



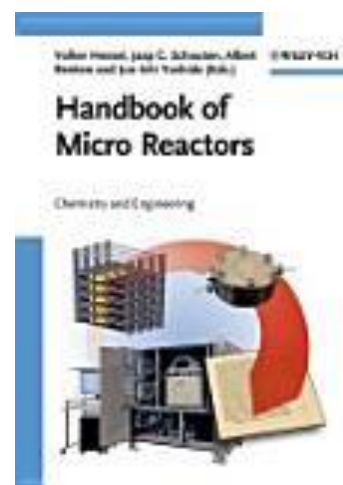
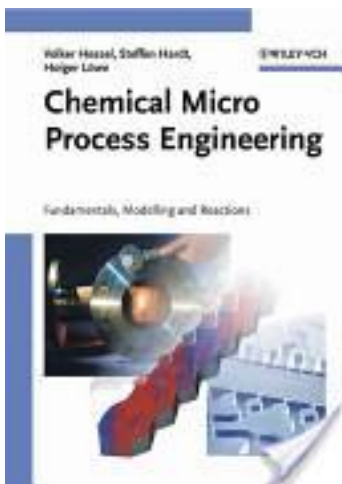
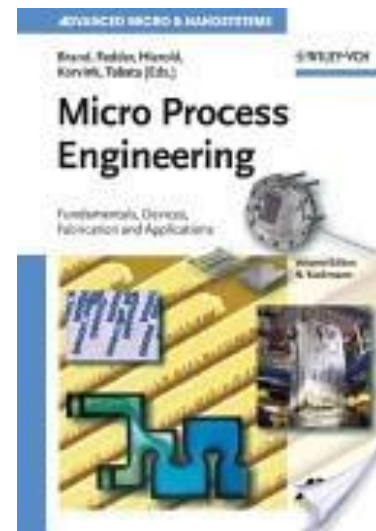
Microfluidic Literature.



Microchemical Journal

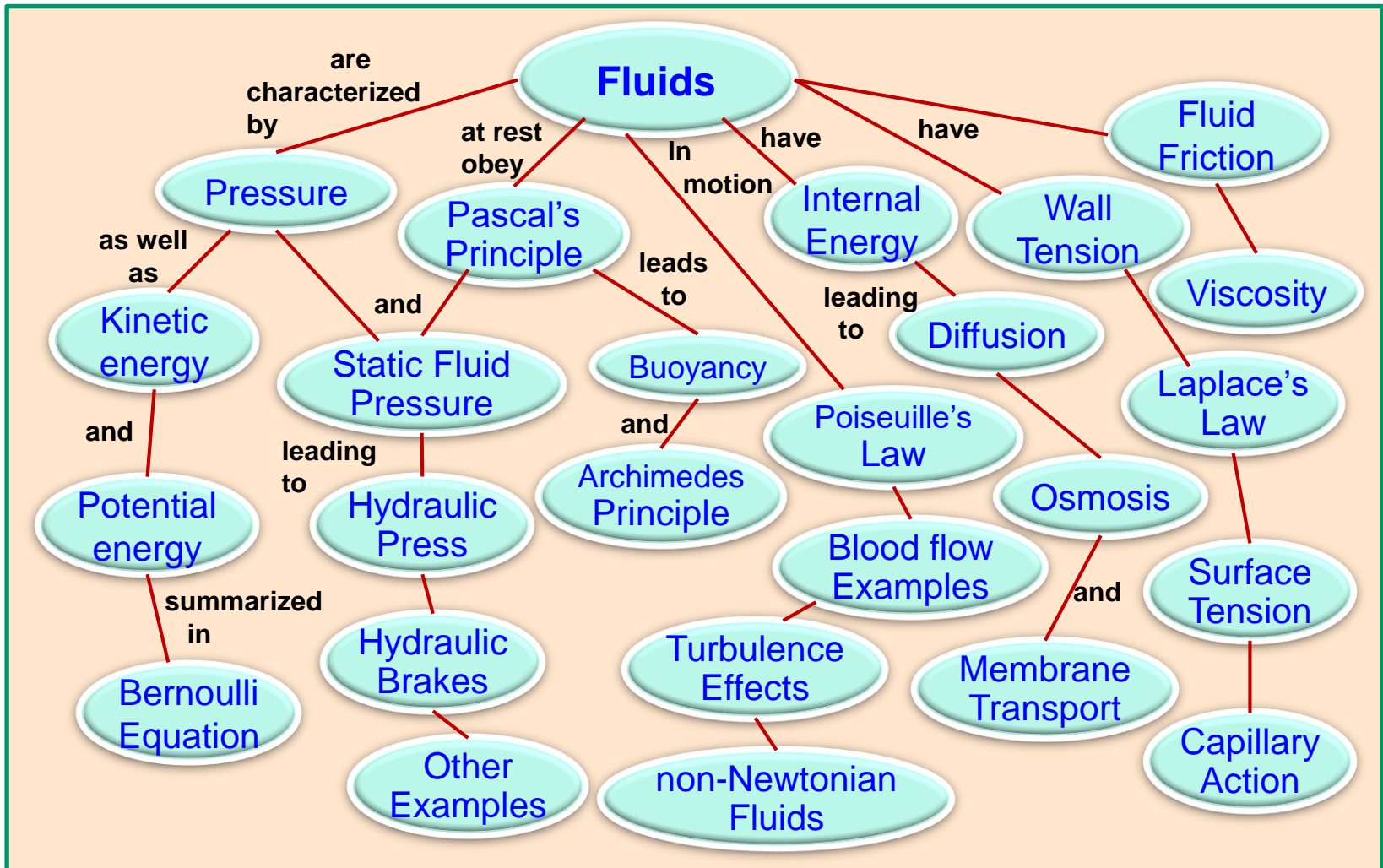


Microreactors Literature.





Literature – Internet.



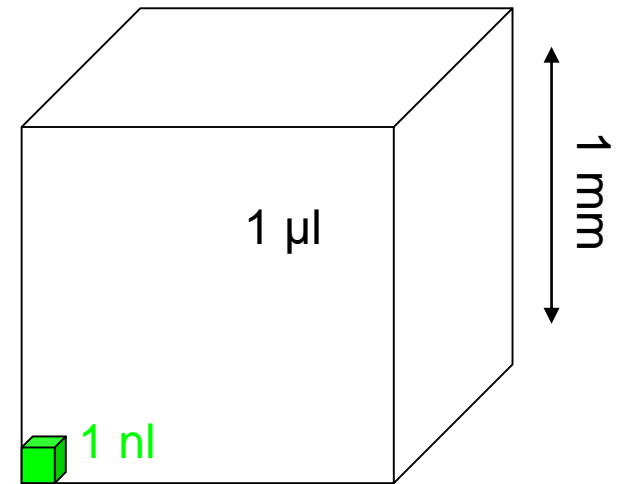


About Microfluidics.

- „Micro“ means at least one of the following features:
 - **small volumes (μl ; nl ; pl ; fl)**
 - small size
 - low energy consumption
 - effects of the micro-domain
 - **Laminar flow**
 - ...



Science Magazine 2 July 1999.



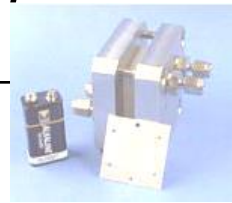


1 nl
1 fl

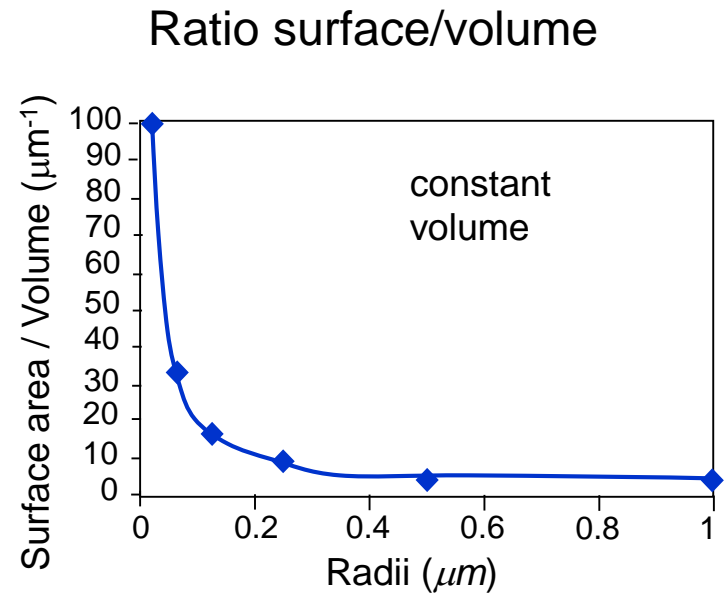
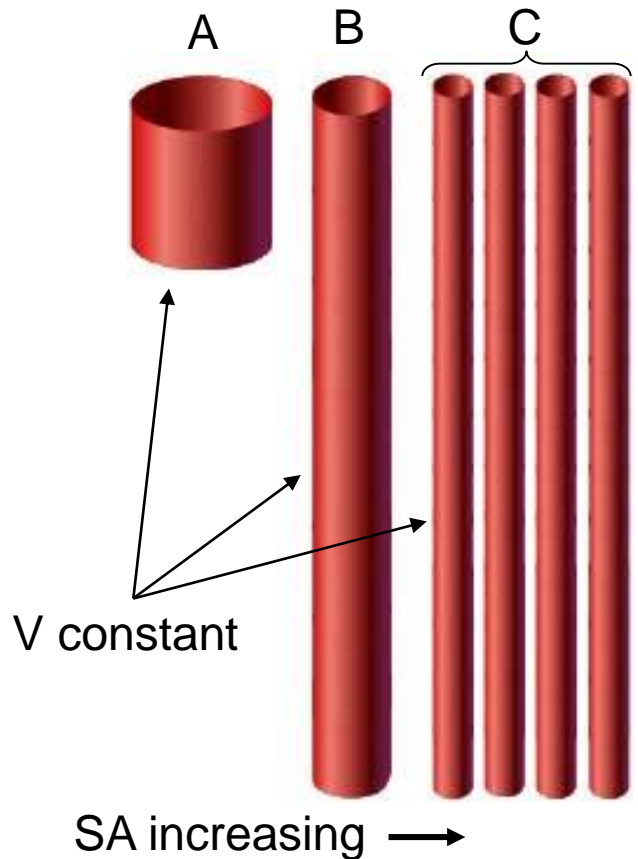
- 1 fl – 1 μl : **10 orders of magnitude**
- still far away from molecular level.



Chemical Reactor Scale.

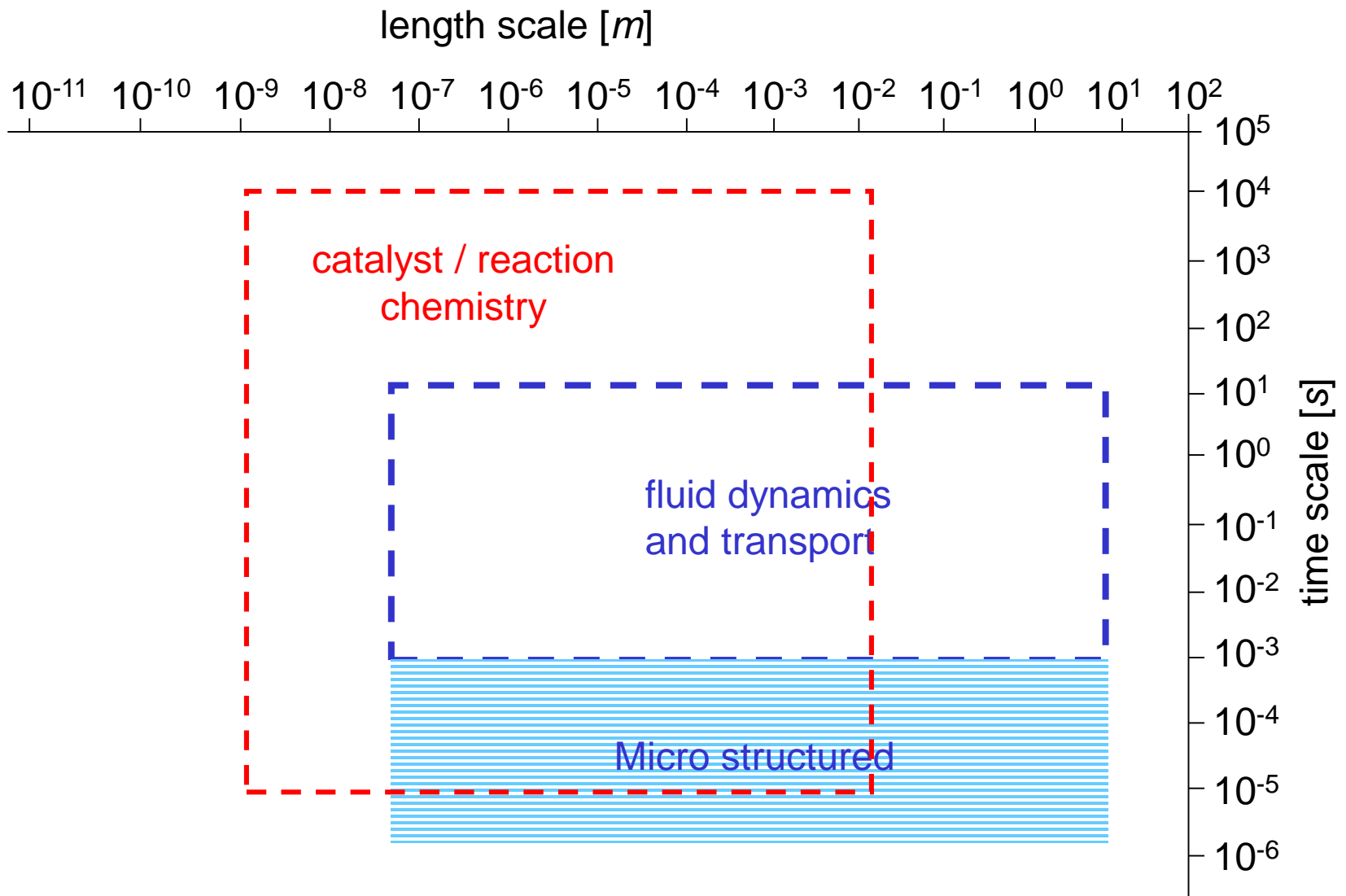
	Industry	Laboratory	Micro-system
Volume	30 m^3	10^{-3} m^3	$3 \cdot 10^{-11} \text{ m}^3$
Scale-down	1 	$1:3 \cdot 10^{-5}$ 	$1:10^{-12}$ 
Diameter	2 m	2 cm	$20 \text{ }\mu\text{m}$
<u>Surface</u> Volume	$2 \frac{\text{m}^2}{\text{m}^3}$	$200 \frac{\text{m}^2}{\text{m}^3}$	$200\,000 \frac{\text{m}^2}{\text{m}^3}$

Key Benefit: Intensified Surface Phenomena by Higher Surface Area-to-Volume Ratios.



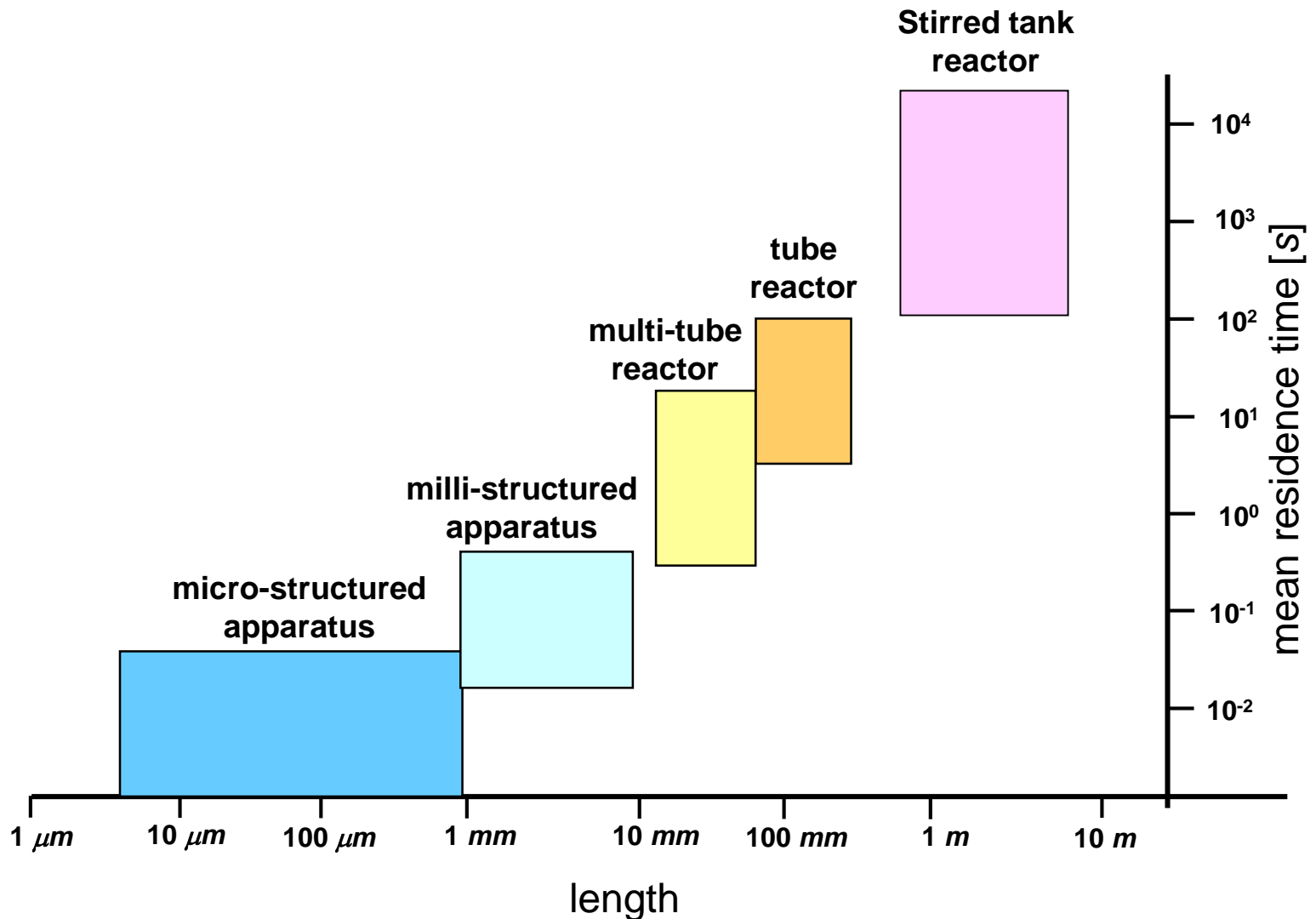
- ***intensified mass transport toward the smaller dimensions***
- ***Intensified heat transport toward the smaller dimensions***
- ***Intensified mixing***
- ***Explosion-Safety improvement***

Length & Time Scale of Chem. & Physical Processes.





Temporal Scale and Typical Length of Chemical Reactors.





Micro-structured Components are Available.

Micro mixers

Mixing from few ml/h
up to 30 l/h



IMM:
Interdigital
micromixer

Micro heat exchangers

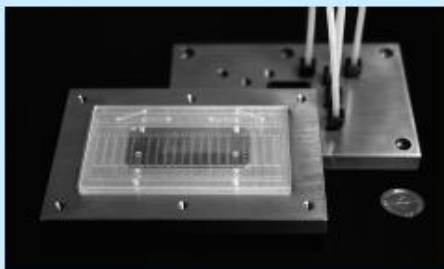
Maximum value of 700 W/m²K
at an air flow rate of 75 l/min



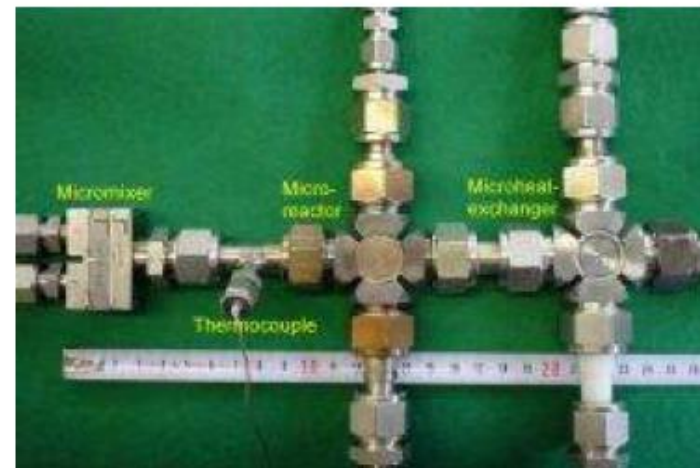
Heatric:
Cross Flow
Heat
Exchanger

Micro reactors

combinaison of μ HE and μ mixers



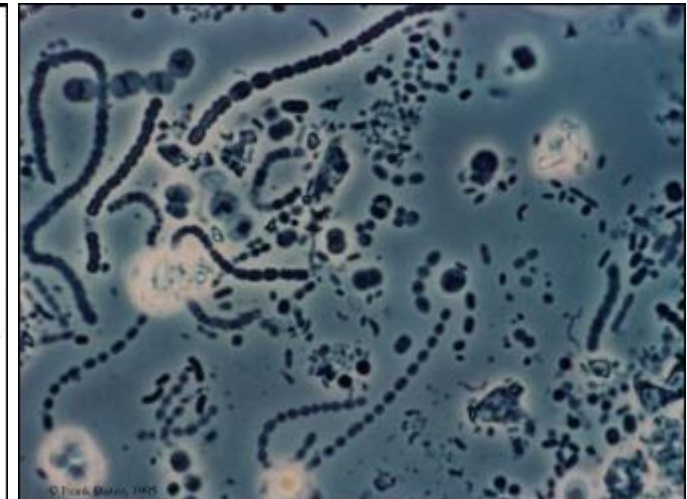
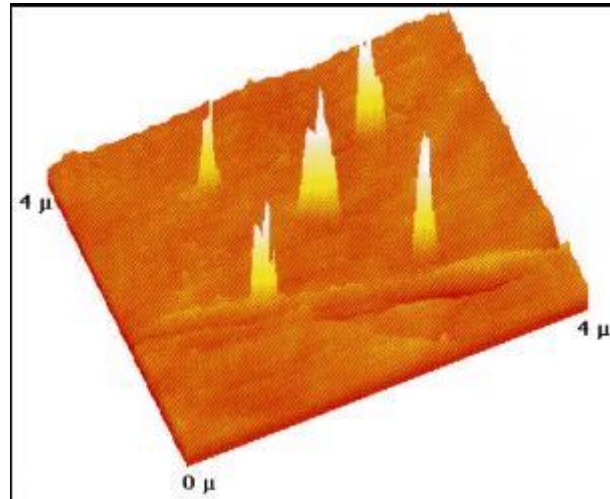
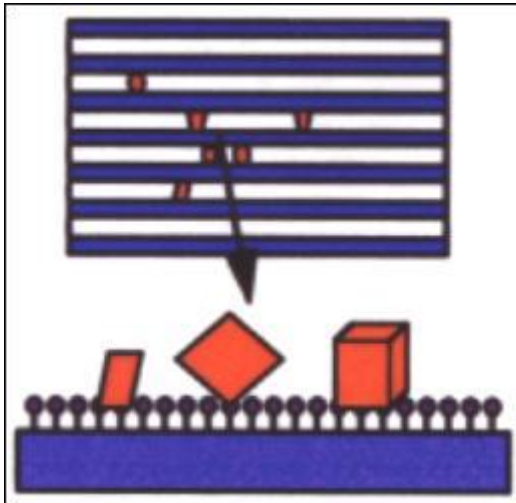
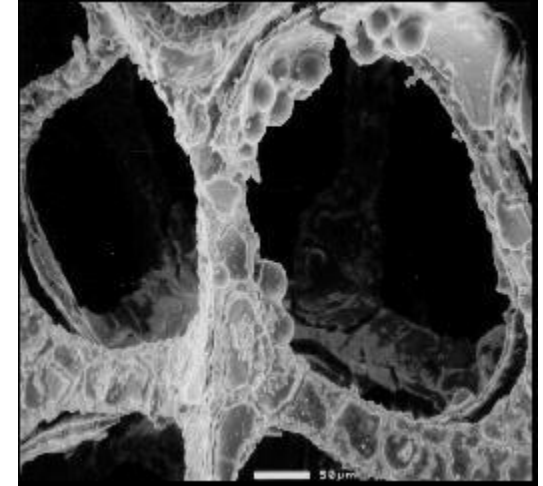
Mikroglas:
Microreact
or





MICRO CHEMICAL AND THERMAL SYSTEMS CONSIDERED AS A “PLATFORM” FOR NANOTECH.

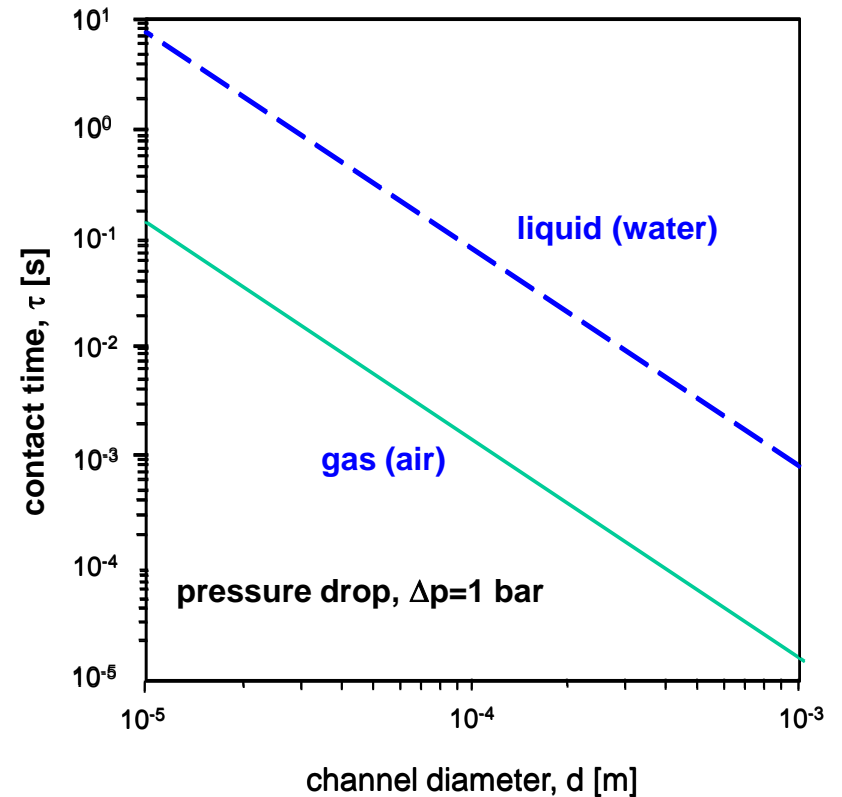
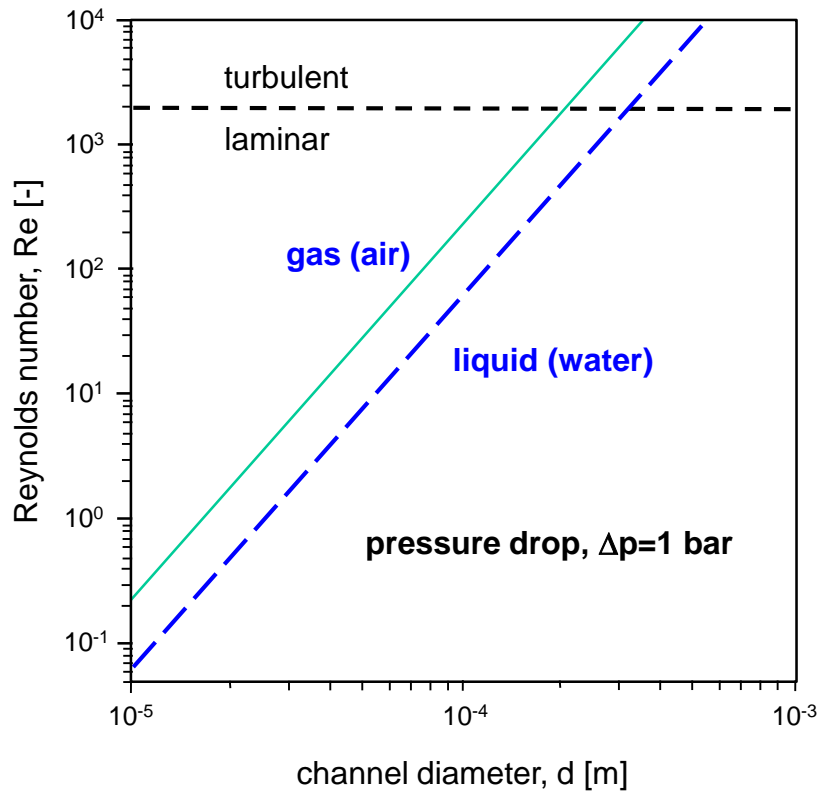
- Engineered structures with improved heat and mass transport
- Self-assembling surfaces
- Nano-fabricated structures
- Biological enzymes as highly functional catalysts





Micro-structured Multichannel Reactor.

Flow conditions for typical fluids, Volume: $V_R = 5 \text{ cm}^3$; $L = 5 \text{ cm}$





Surface to Volume: Effective Transport.

Example: overall heat transfer coefficient.

<i>Type Hx</i>	<i>U (W·m⁻²·K⁻¹)</i>
Tubular	150-1200
Spiral	700-2500
Laminar	1000-4000

Micro-channel: **3800-6800 W·m⁻²·K⁻¹**



(500×500 μm^2 × 1.5 cm channels)



Properties of Micro Devices.

- **Behavior of fluids at this scale**
 - Wall effects dominate
- **Surfaces and interfaces**
 - Fouling
 - Multi-phase flow
 - Surface energy, tension, wettability
 - Dynamics -- start-up
- **Equipment**
 - Basic state measurements - P , T , phase, quality, composition
 - Density, thermal conductivity, electrical conductivity
 - Controls -- need to be integrated
 - Fluid flow and distribution
 - System homogeneity



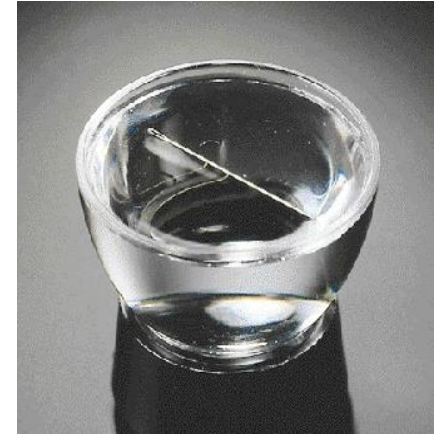
About Microfluidics (2).

- „Micro“ means at least one of the following features
 - small volumes (μL ; $n\text{L}$; $p\text{L}$; $f\text{L}$)
 - small size
 - low energy consumption
 - **effects of the micro-domain**
 - Laminar flow
 - Surface tension



Surface Tension γ : $\gamma = \frac{dw}{dS}$

(work to be made to increase the surface of a unit quantity)



Cohesive forces bind molecules each other.

Adhesive forces bind molecules to surface.

Compound :	$n\text{-C}_6\text{H}_{14}$	H_2O	Hg
γ ($\text{mN}\cdot\text{m}^{-1}$):	18.4	72.8	425.4



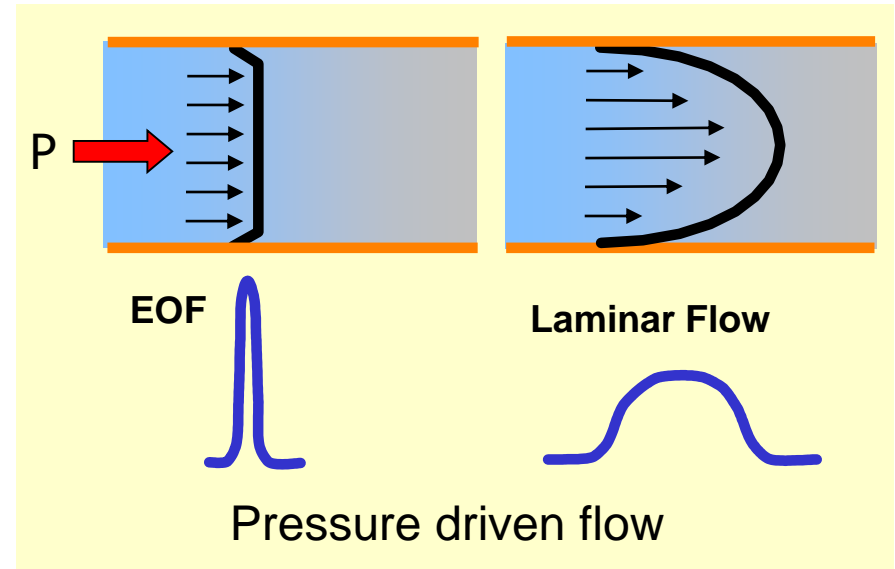
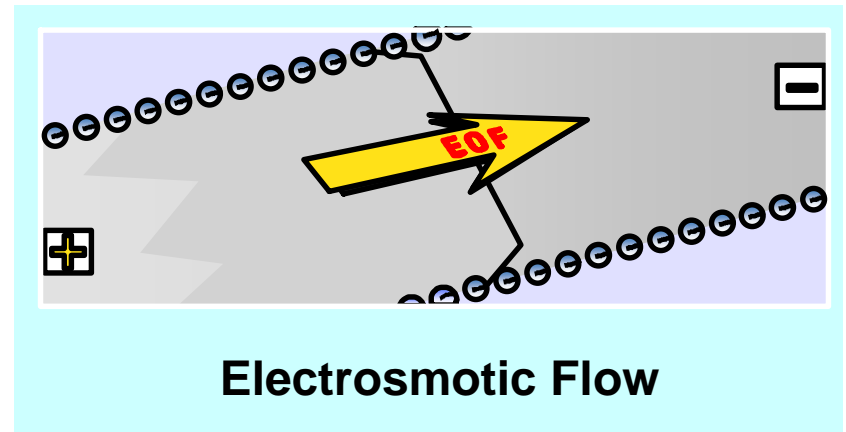
About Microfluidics (3).

- „Micro“ means at least one of the following features
 - small volumes (μl ; nl ; pl ; fl)
 - small size
 - low energy consumption
 - **effects of the micro-domain**
 - **Laminar flow**
 - Surface tension
 - **electrical surface charges**
 - diffusion

Reynolds
Number
< 2300

$$Re = \frac{u\rho L}{\eta}$$

velocity u , density ρ , traveled length L , and viscosity η of the fluid





Market for Microfluidics.

Printing

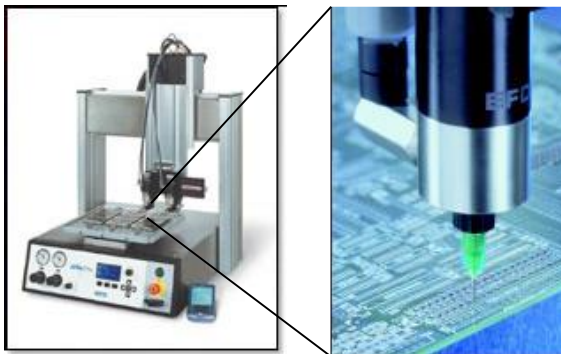


Industrial Automation

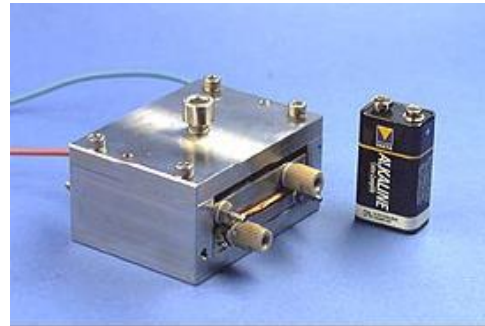


**Flow sensors for
air conditioning
(HSG-IMIT)**
50.000 units in 2005

Industrial dispenser



Chem Process Engineering/ Power systems

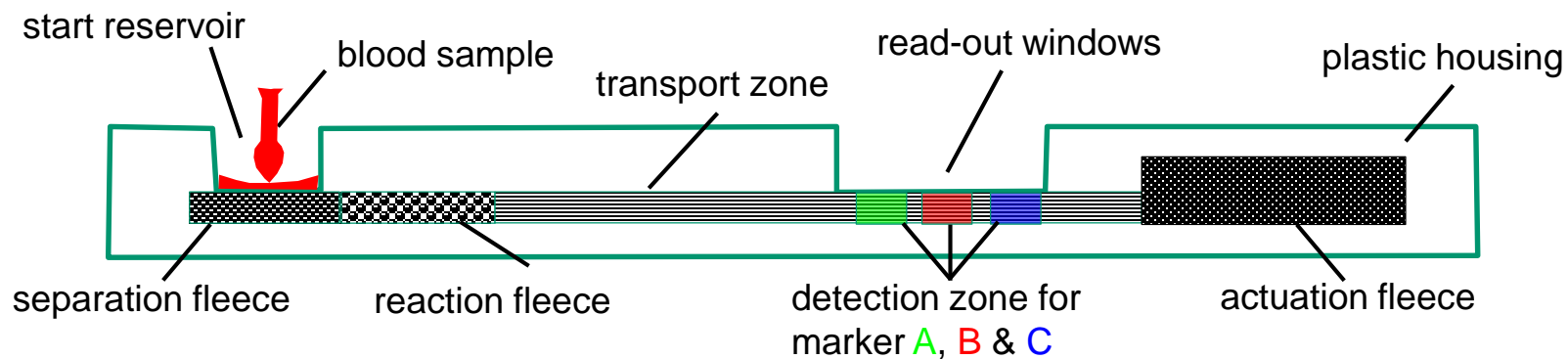
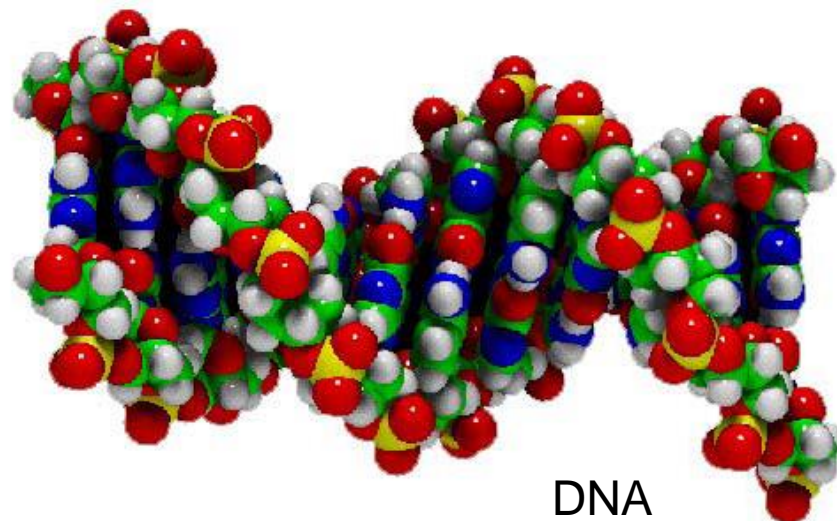




Market for Microfluidics (2).

Life Sciences!!!!

- Capillary Electrophoresis
- Lab on chip
- Drug delivery
- Clinical analysis

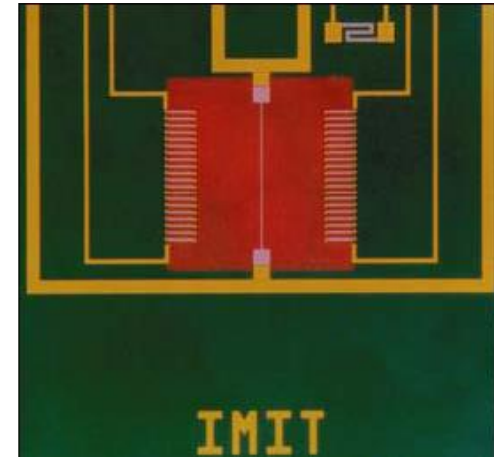




Flow Sensors.

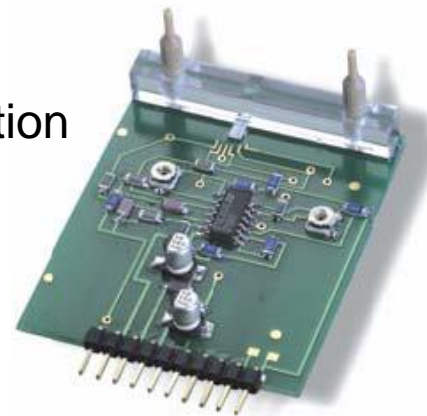
Working principle:

- Thermal principles
- Heaters & temperature sensors
 - Anemometer
 - Calorimeter
 - Time of flight



Specifications:

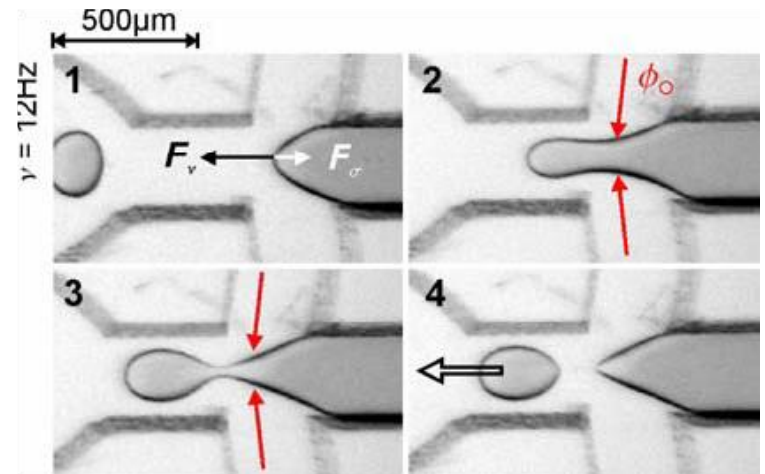
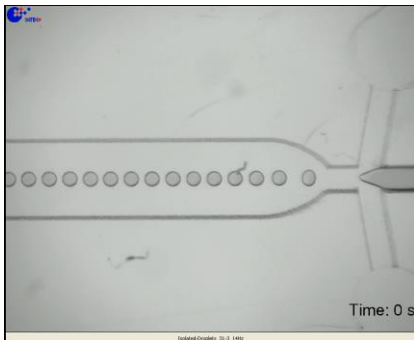
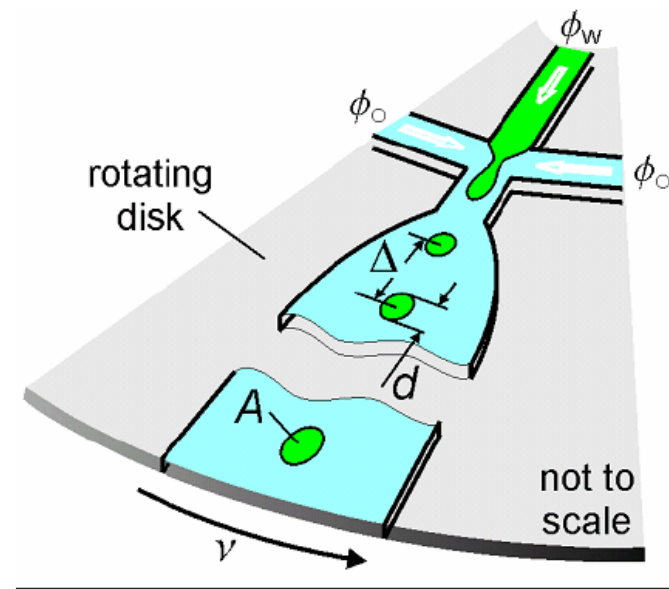
- Range: $15 \mu\text{m/s} - 1500 \mu\text{m/s}$
- Power: $< 15 \text{ mW}$
- Response time: $< 1 \text{ ms}$
- Application specific configuration possible by adaption of flow channels





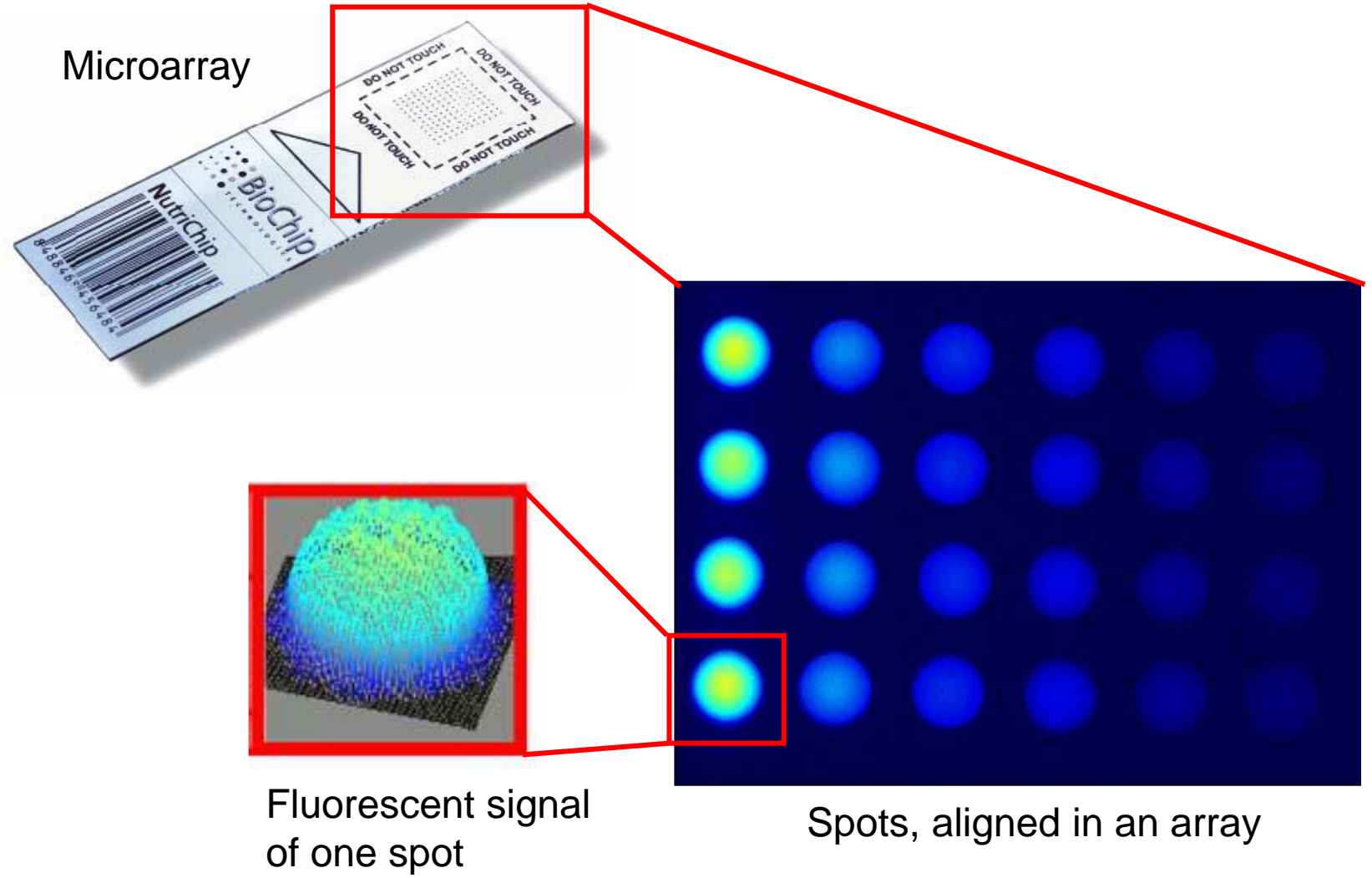
Lab-on-a-Chip: *Emulsion-Disk*.

- Controlled droplet generation on rotating disk
- Water-plug is focused by two oil flows ϕ_0
- Production of water-droplets in oil (W/O emulsion)
 - Volume: **5...22 nL**
 - Rate: 0...300 *drops / s*
- High Reproducibility
 - Droplet diameter: **CV < 2%**





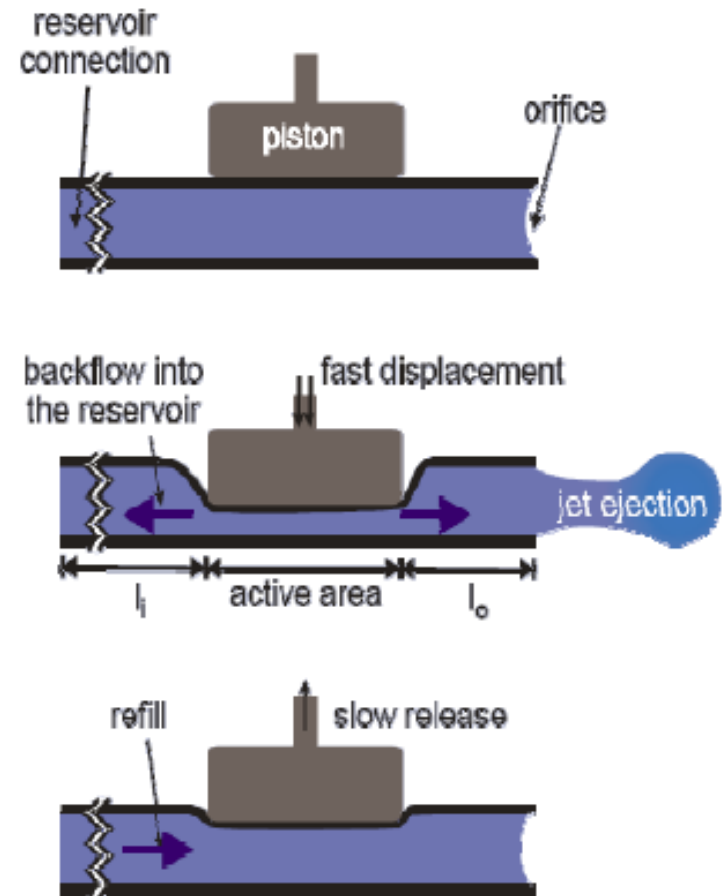
DNA Microarray Printing.





PipeJet Principle.

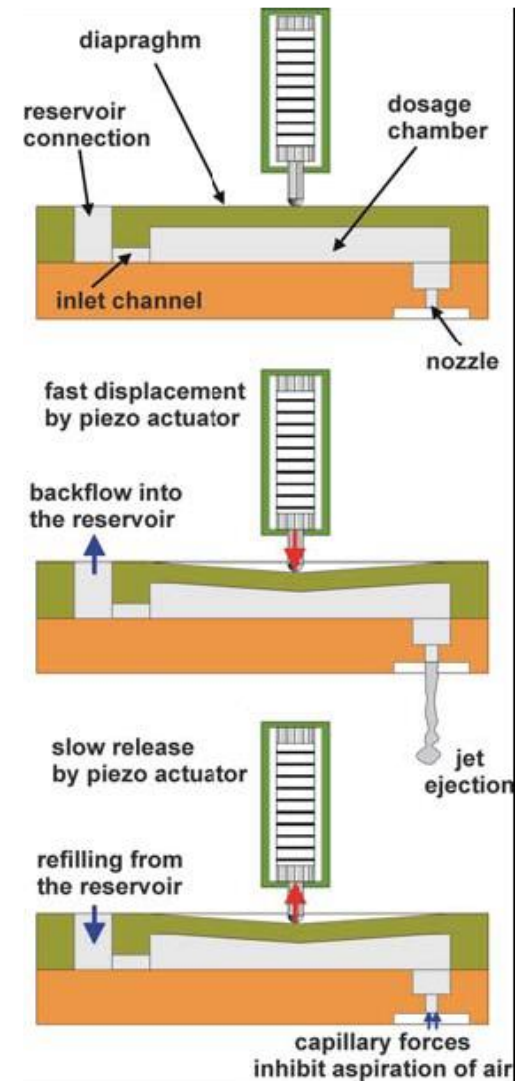
- **Dispensing by direct volume deflection**
 - Polymer tube
 - Piezo-actuated piston
 - Fast displacement for jet ejection
 - Short plateau
 - Slow release for capillary refill
- **Unique strength of concept**
 - Contact-free delivery of fluid
 - Simplest possible fluidic geometry
 - Easiest packaging (mechanical clamping).





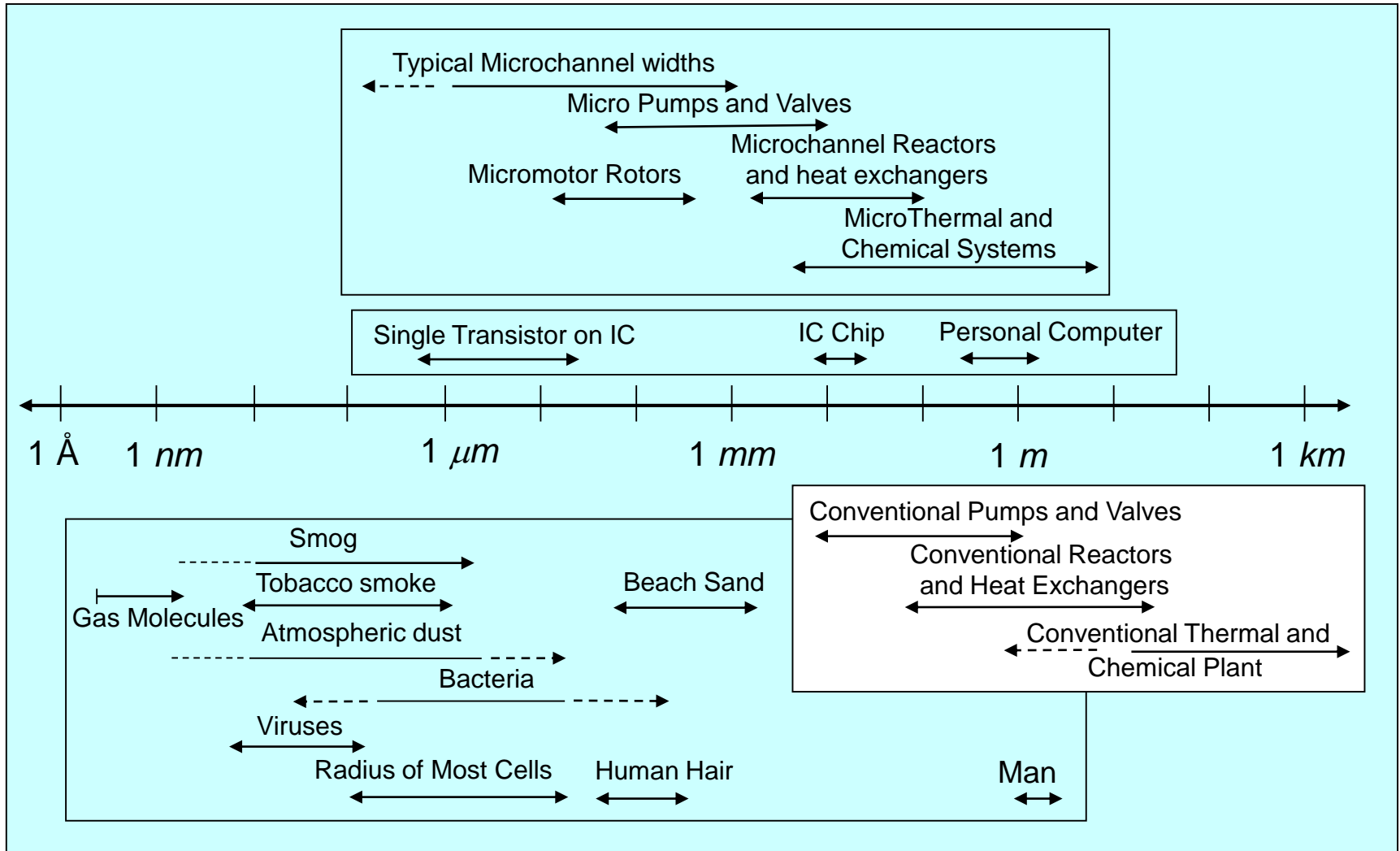
nL & pL Dosage: NanoJet.

- Dosage volume: 5 nL to 1.000 nL
- Dosage rate: 1.000 nL/s
- Viscosity range: $1 - 100 \text{ mPas}$
- Precision: better 5 %





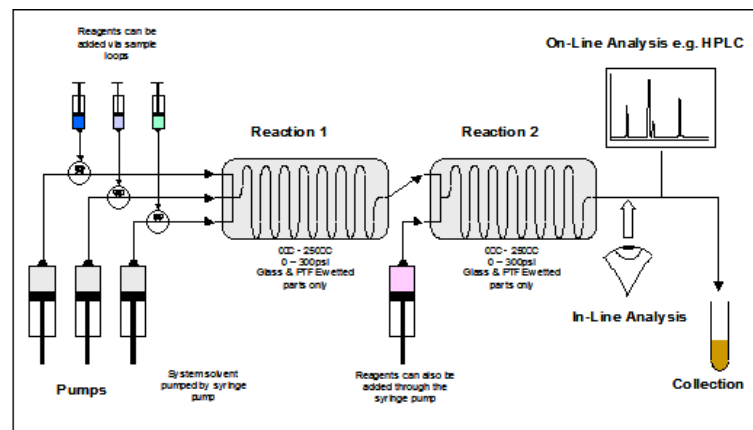
A New Class of Process Technology.





Features of a Continuous Microreactor System.

1. Precise control of temperature – easily set and changed - **no temperature gradients**
2. Precise control of time - easily set and changed – **quick hot reactions for consistent particle size**
3. Precise control of feeds/stoichiometry – **rapidly investigate stoichiometry by changing feed rates**
4. Consistent and rapid mixing – **ensures nucleation not precipitation**
5. No scale limitations – **small scale for optimisation; or “leave tap running” to make kilograms per day (100 g/h readily achievable)**
6. Reproducible – **same temperature, same mixing, same reaction time, every time**
7. Immediate aqueous work up – **simple work up available if required**



Tice, J.D. et al. Langmuir 2003 19, 9127-8133

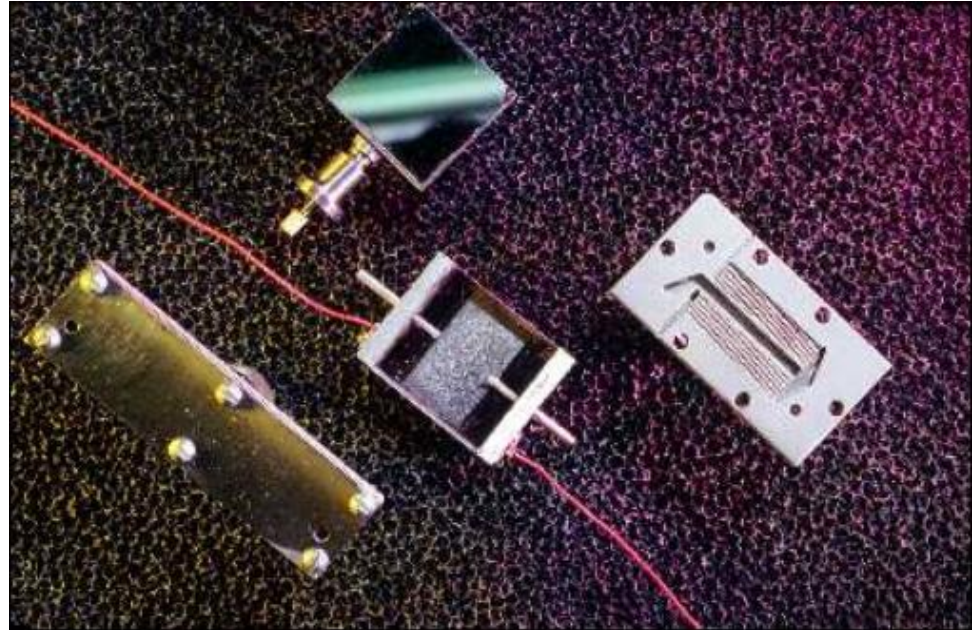


Micro Chemical Equipments and Systems.

- Microreactors
- Micro-channels
- Micro heat exchangers,
- Micromixers
- Separation Units and
- Micro analytical devices

Miniaturization:

- High capacity
- Light systems
- Mass manufacture
- Costly but versatile

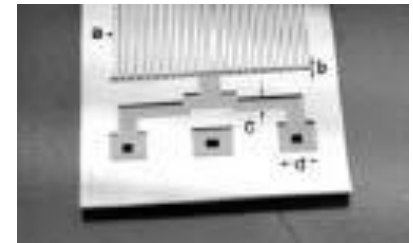
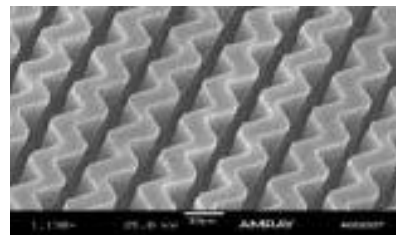
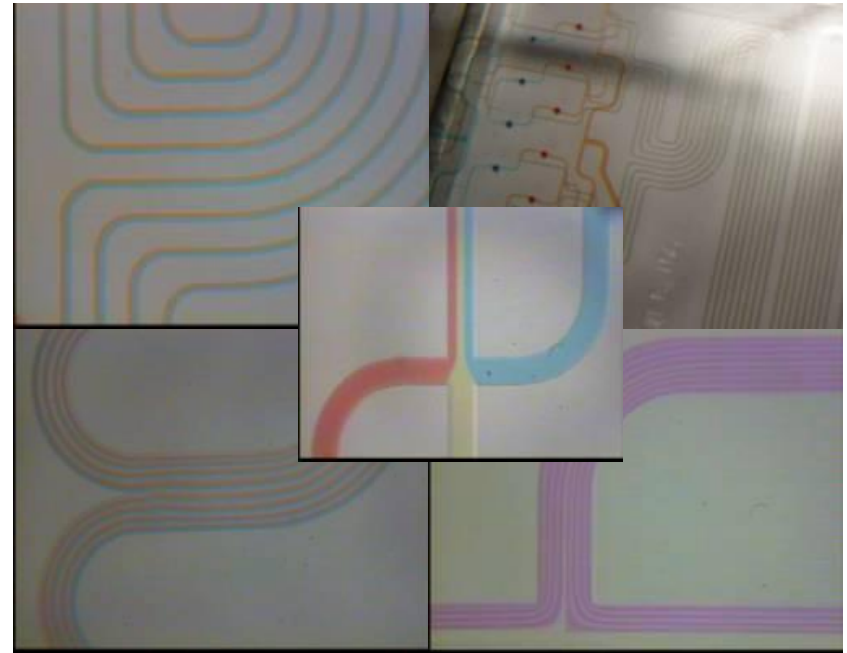


MEMS, Mesoscopic Machine
Micro/Nano Systems
Microcats



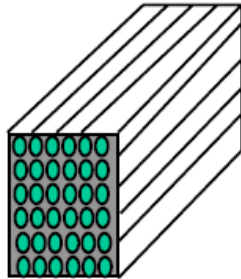
Micro-Reactors.

- New reactor types which offer high capacity and high productivity.
- Microreactors are more versatile and less dependent on chemical-engineering operators
 - Provide useful amount of products
 - Are easy to use.





Micro-structured Multichannel Reactors.



Volume: $V_R = 5 \text{ cm}^3$

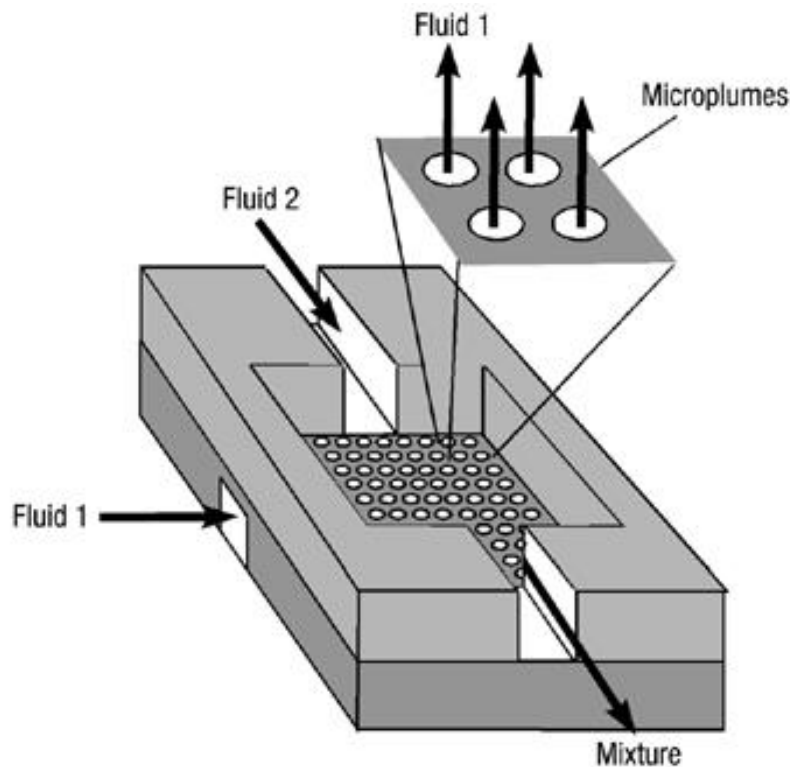
Pressure drop: $\Delta p = 1 \text{ bar}$



length:	$L=$	5.	cm
diameter:	$d=$	100.	μm
Number of channels:	$N=$	12,740.	
Specific surface:	$a=$	40,000.	m^2/m^3
Flow velocity:	$u=$	0.63	m/s (water)
		35.	m/s (air)
Mass flow:	$Q_m=$	225.	kg/h (water)
		15.	kg/h (air)



Injection of Multiple Microjets



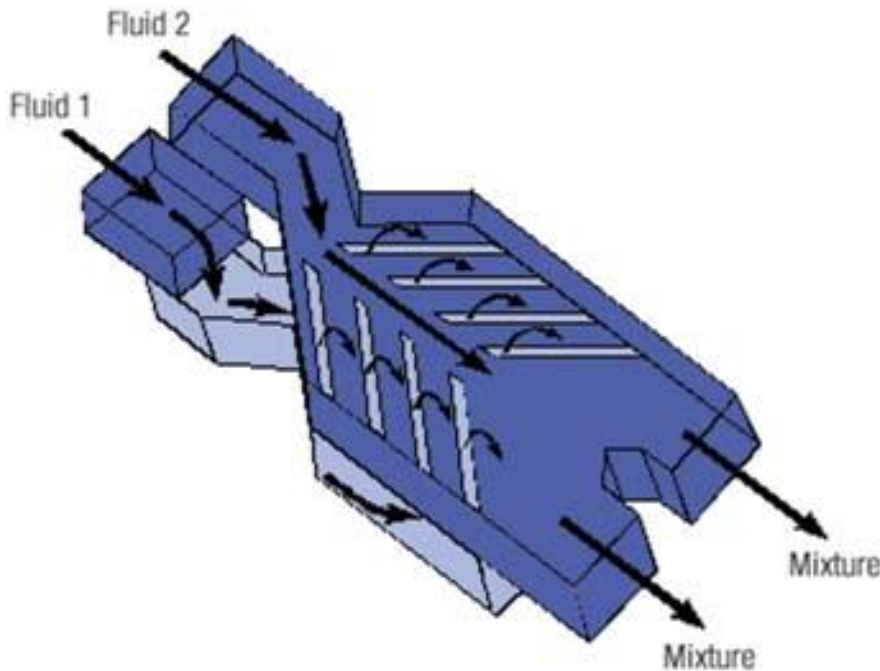
Schematic of a micromixer with injection of multiple microjets into a mixing chamber

1. The central element of the mixer is a sievelike structure with a large number of regular holes.
2. During operations, the mixing are is filled with one liquid, and the other liquid is injected into the mixing volume through a multitude of microholes.
3. Numerous microjets are generated and increase the contact surface between the two liquids.
4. The holes are positioned in rows 10-100 μm apart, which results in short diffusional paths between the jets.
5. Typical flowrates are in the $\mu\text{L/s}$, the hole diameter is 10 μm , and the height of the mixing chamber some 100 μm

Source: Quak Foo Lee



Multiple Flow Splitting and Recombination



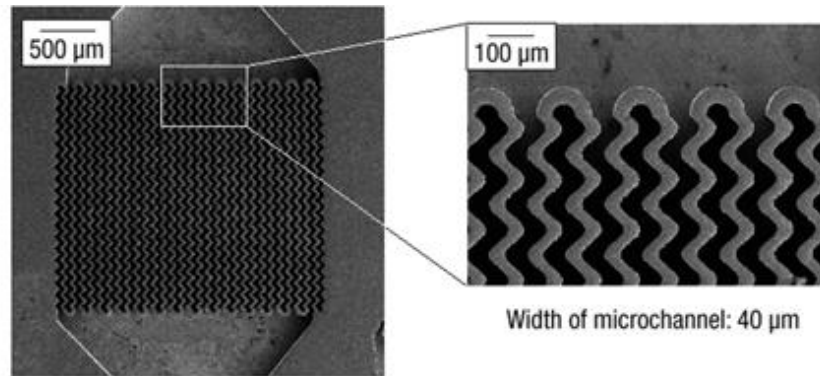
Mixing units of a static micromixer with multiple slit-shaped injection openings

1. Application: industrial chemical sensor
2. Flow range: 0.01 – 0.1 $\mu\text{L/s}$
3. Highly viscous flow with a $\text{Re} < 1$
4. The whole system consists of a silicon/glass sandwich connected by anodic bonding.
5. One channel structure is etched into glass and the other into silicon.
6. In the region where the channels overlap, they are separated by a structured plate defined by an etchstop layer.
7. Max. width = 300 μm
max. depth = 30 μm
8. The thickness of the structured plate for separating the channels in the glass and the silicon wafer is 5 μm and the slit width 15 μm .

Source: Quak Foo Lee

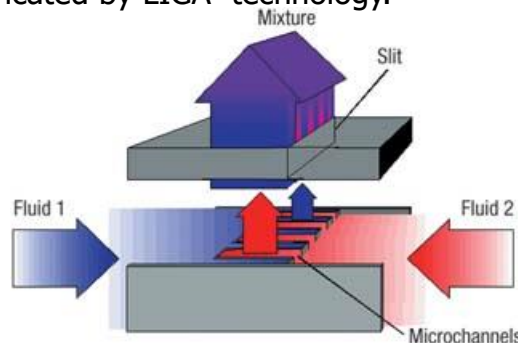


Multilamination of Fluid Layers



Mixing element with 2 x 15 microchannels

Scanning electron micrographs of a mixing element based on multilamination of thin fluid layers. The device consists of 2 × 15 interdigitated microchannels with corrugated walls, fabricated by LIGA technology.



Multilamination of streams in channels with corrugated walls, leading to fast mixing by diffusion.

1. The fluid to be mixed are introduced into the mixing elements in counter-flow and stream into an interdigitated channels with corrugated walls.
2. Typical channel widths = 25 or 40 μm
3. The channel configuration leads to a periodical arrangement of flow lamellae of the two fluids.
4. The lamellar flow leaves the device perpendicular to the direction of the feed flows and, because of the thinness of the lamellae, fast mixing takes place by diffusion.
5. The corrugated channel walls increase the contact surface of the lamellar streams and improve the mechanical stability of the separating walls.

Source: Quak Foo Lee



Gasoline Vaporizer.



1999 - R&D Award Winner

- 50 kW_e capacity: Four cells each of microchannel reactors and heat exchangers
- Volume: 0.3 L
- Processes/combusts 1400 SLPM



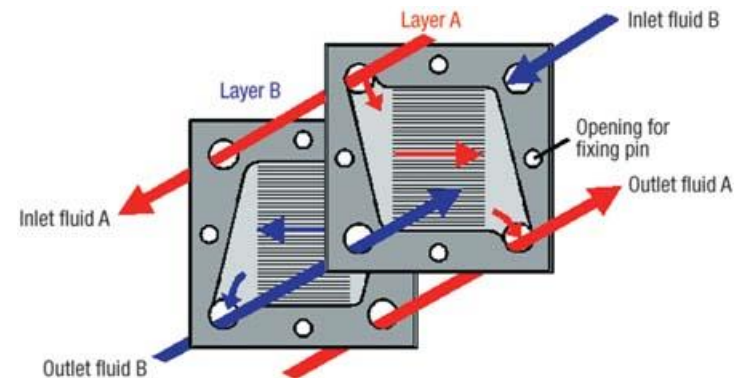
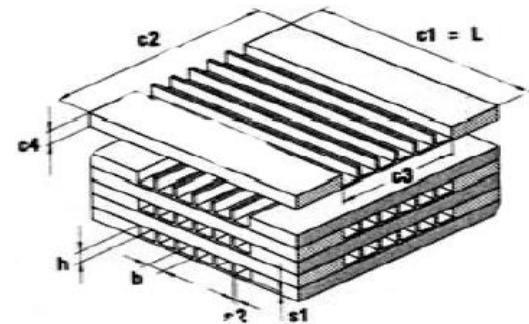
Micro Heat Exchangers.

Cross-Flow Heat Exchange in Stacked Plate Devices



Channel diameter: $\sim 50 - 500 \mu\text{m}$
Channel length: $20 - 100 \text{ mm}$
No of channel: $200 - 1000$
Specific surface: $10^4 - 10^5 \text{ m}^2/\text{m}^3$

Micro heat exchanger with connections for fluid supply
(source: Forschungszentrum Karlsruhe)

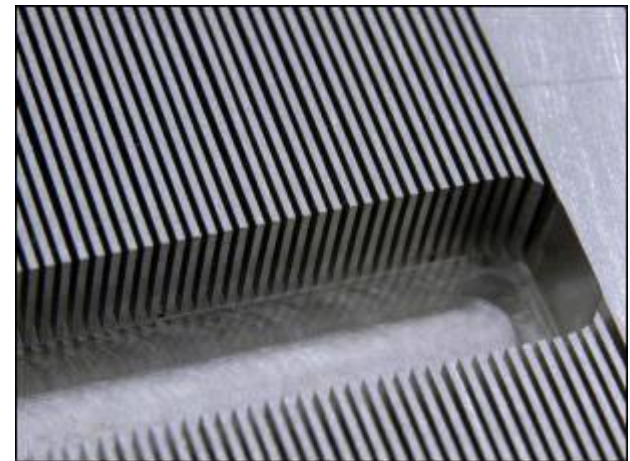
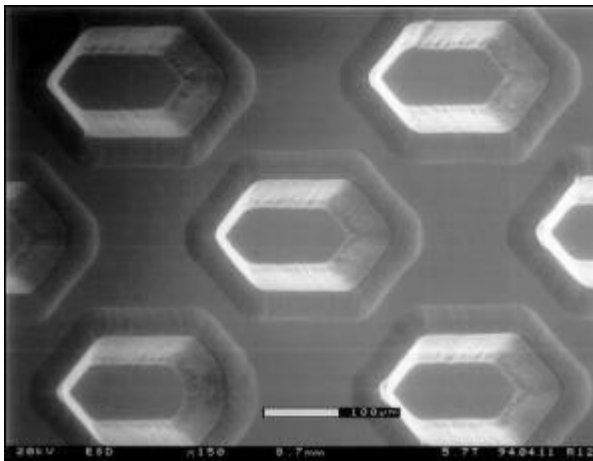
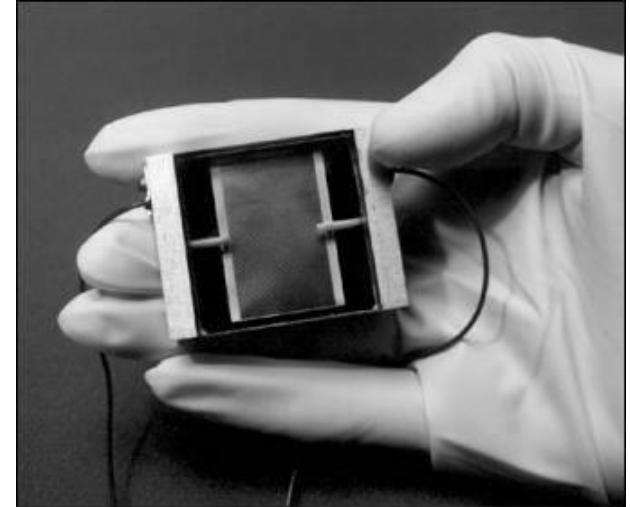


Counterflow Heat Exchange
in Stacked Plate Devices



Advantage: Rapid Heat and Mass Transport Microchannel Heat Exchangers.

- Heat fluxes: 100+ watts/cm²
- Low pressure drops: 1-2 psia
- High convective heat transfer coefficients
 - Liquid phase: 10,000 - 15,000 W·m⁻²·K⁻¹
 - Evaporating phase: 30,000 - 35,000 W·m⁻²·K⁻¹

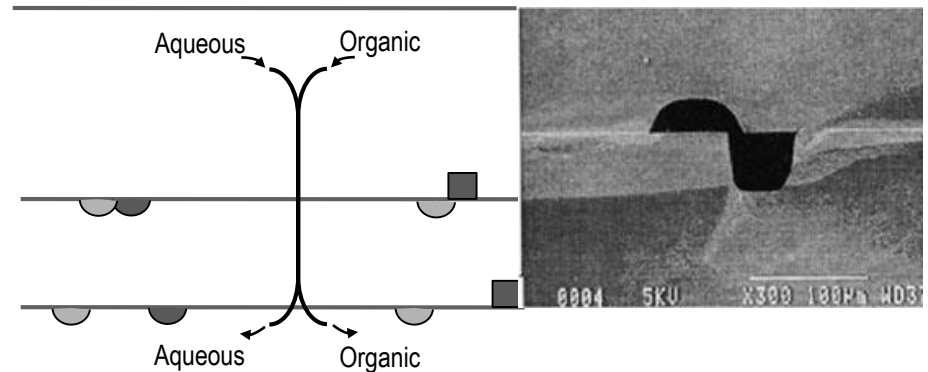




Microseparators.

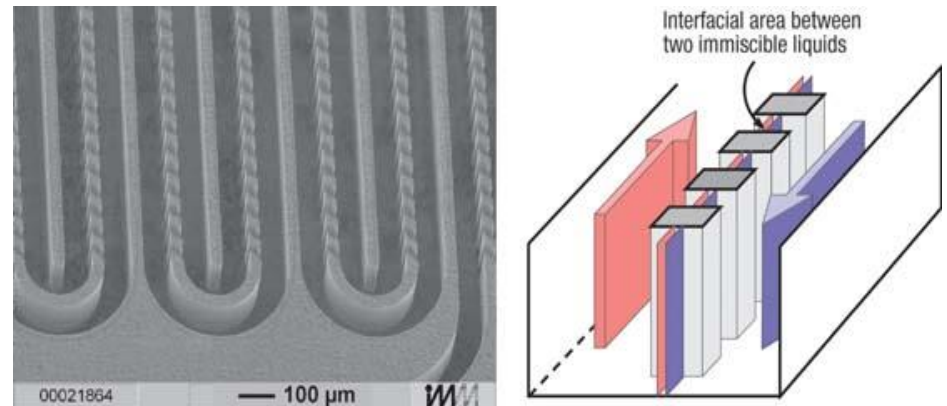
Exchange between Immiscible Fluids

Schematic of solute exchange between immiscible fluids in partially overlapping microchannels (left) and scanning electron micrograph of the cross section of the partially overlapping microchannels (right),



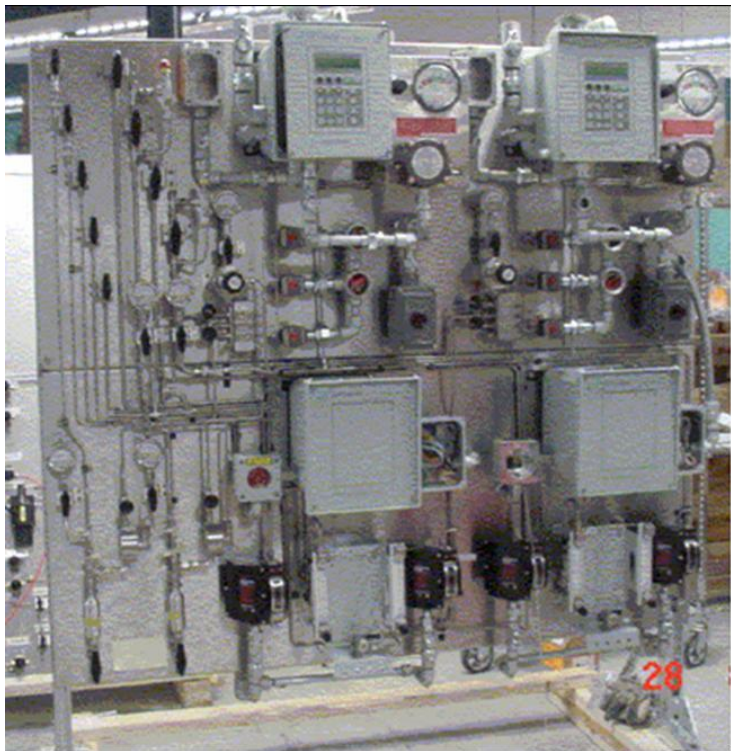
Exchange between Immiscible Fluids

Scanning electron micrograph (left) and schematic (right) of an extraction unit with adjacent channels for two fluids with slits, oblique to the flow direction, for exchange between the two phases.





Miniaturization of Analytical Systems.



Traditional System



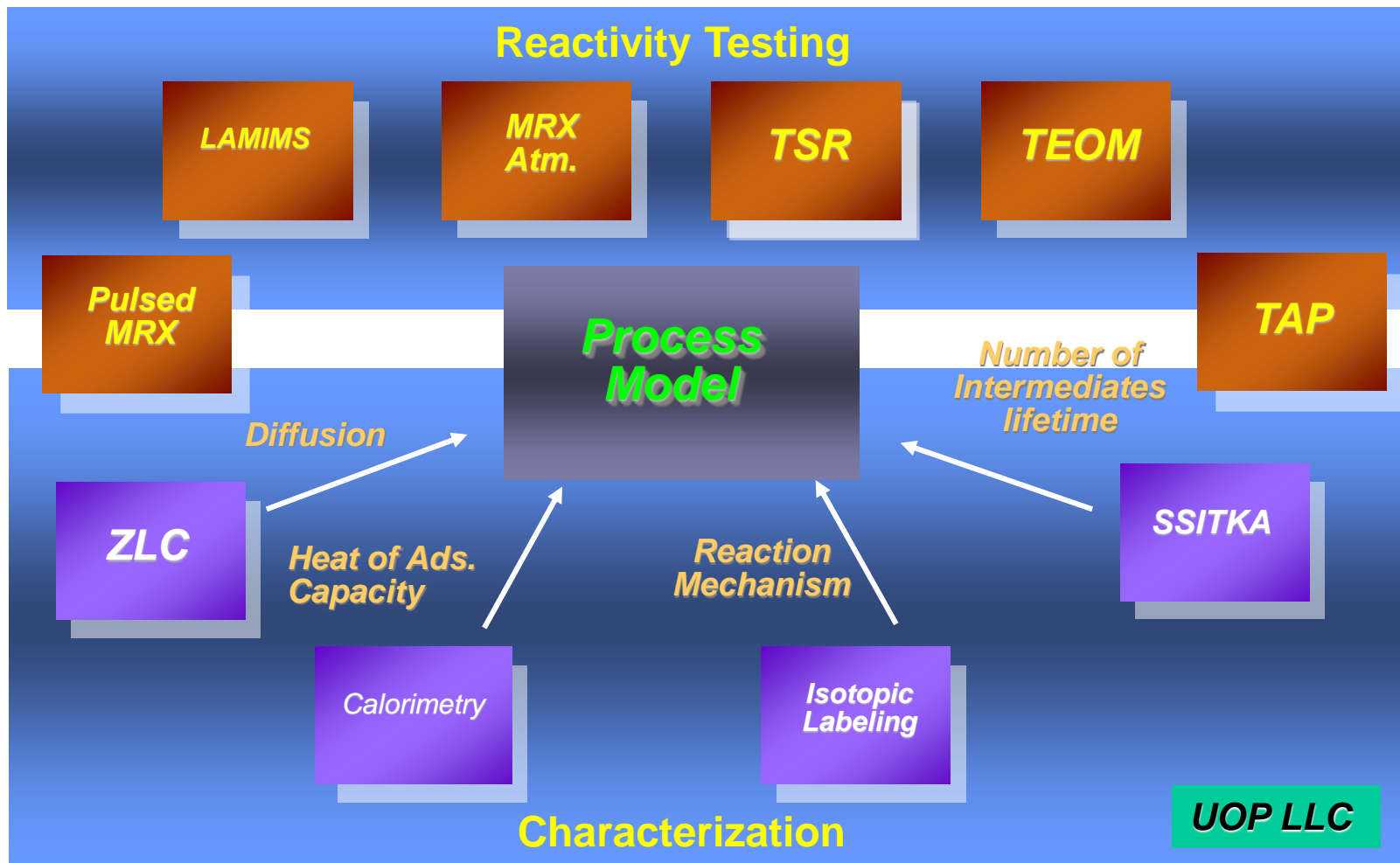
UOP LLC



NeSSI system

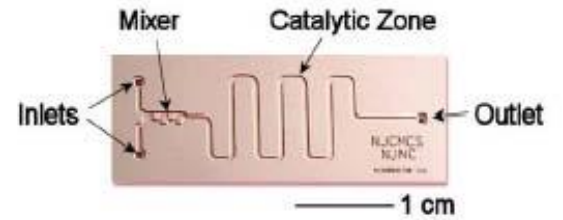
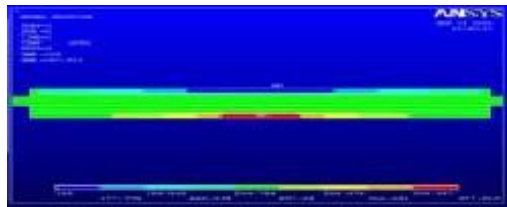
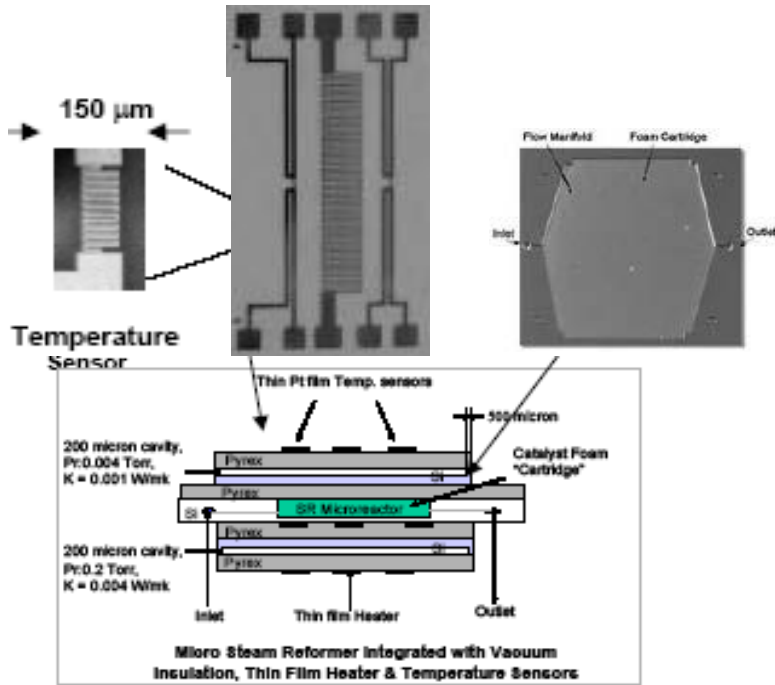


Mechanism Tools.

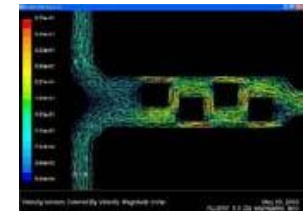
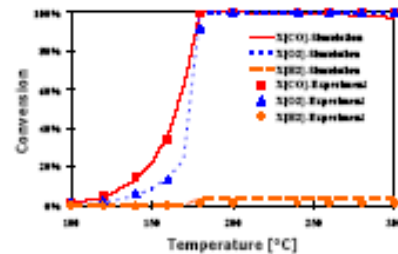
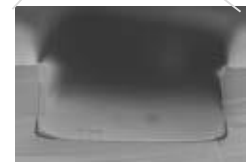
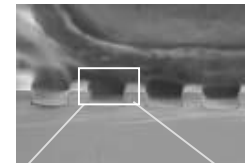




CPM – H₂ Production.

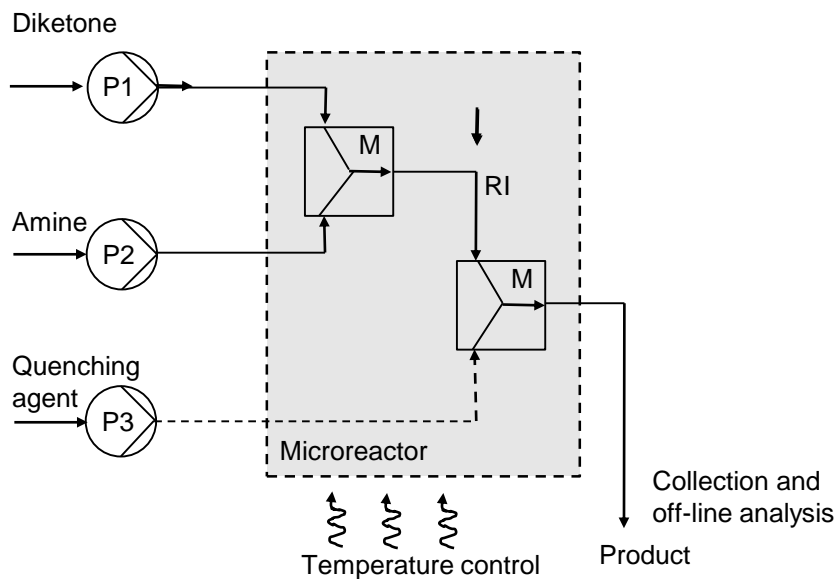
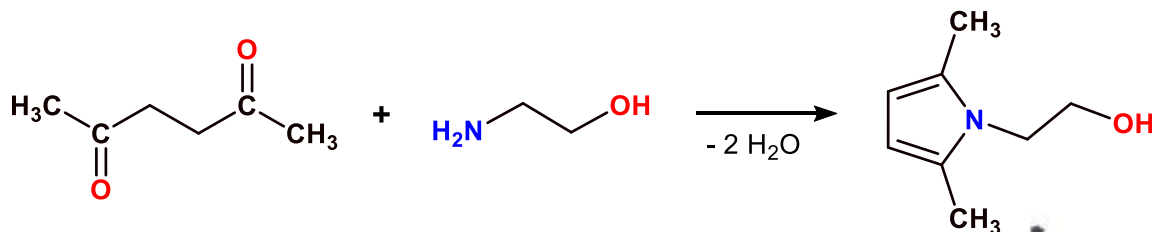


- | | |
|---|---|
| 1. $2\text{H}_2 + \text{Pt} \rightarrow \text{H}_2 + \text{H}_2$ | 15. $\text{CH}_4 + \text{Pt} \rightarrow \text{H}_2 + \text{CO}$ |
| 2. $\text{C}_2\text{H}_6 + \text{Pt} \rightarrow \text{C}_2\text{H}_4 + \text{H}_2$ | 16. $\text{H}_2\text{O} + \text{Pt} \rightarrow \text{H}_2 + \text{O}$ |
| 3. $\text{H}_2 + \text{Pt} \rightarrow \text{H} + \text{H}$ | 17. $\text{CH}_4 + \text{O}_2 \rightarrow \text{CO} + \text{H}_2\text{O}$ |
| 4. $\text{CO} + \text{Pt} \rightarrow \text{CO}_2$ | 18. $\text{H}_2\text{O} + \text{O}_2 \rightarrow \text{H}_2\text{O}_2 + \text{O}_2$ |
| 5. $\text{CO} + \text{H}_2 \rightarrow \text{COH}$ | 19. $\text{H}_2\text{O} \rightarrow \text{H}_2 + \text{O}$ |
| 6. $\text{CO}_2 \rightarrow \text{CO} + \text{O}$ | 20. $\text{H}_2 \rightarrow \text{H} + \text{H}$ |
| 7. $\text{CO}_2 \rightarrow \text{CO} + \text{O}_2$ | 21. $\text{O} + \text{H}_2 \rightarrow \text{H}_2\text{O}$ |
| 8. $\text{O}_2 + \text{Pt} \rightarrow \text{O} + \text{O}$ | 22. $\text{O}_2 \rightarrow \text{O} + \text{O}$ |
| 9. $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$ | 23. $\text{O} + \text{H}_2\text{O} \rightarrow \text{H}_2 + \text{O}_2$ |
| 10. $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$ | 24. $\text{O} + \text{H}_2 \rightarrow \text{H} + \text{OH}$ |
| 11. $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$ | 25. $\text{H}_2 + \text{O} \rightarrow \text{H} + \text{OH}$ |
| 12. $\text{CO}_2 + \text{H}_2 \rightarrow \text{CO} + \text{H}_2\text{O}$ | 26. $\text{O}_2 + \text{H}_2 \rightarrow \text{H}_2\text{O} + \text{O}$ |
| 13. $\text{CO}_2 + \text{H}_2 \rightarrow \text{CO} + \text{H}_2\text{O}$ | 27. $\text{H}_2\text{O} \rightarrow \text{H}_2 + \text{O}$ |
| 14. $\text{H}_2 + \text{O}_2 \rightarrow \text{H}_2\text{O} + \text{O}$ | 28. $\text{H}_2 + \text{O}_2 \rightarrow \text{H}_2\text{O} + \text{O}$ |

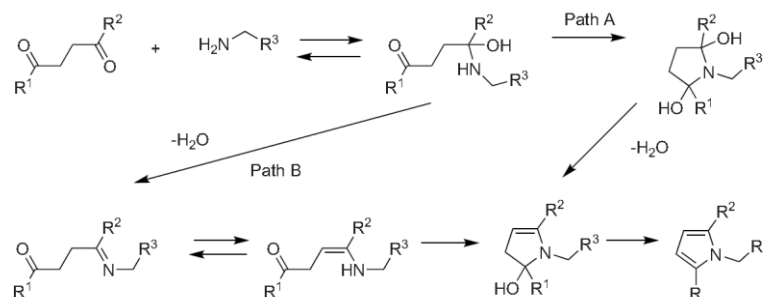




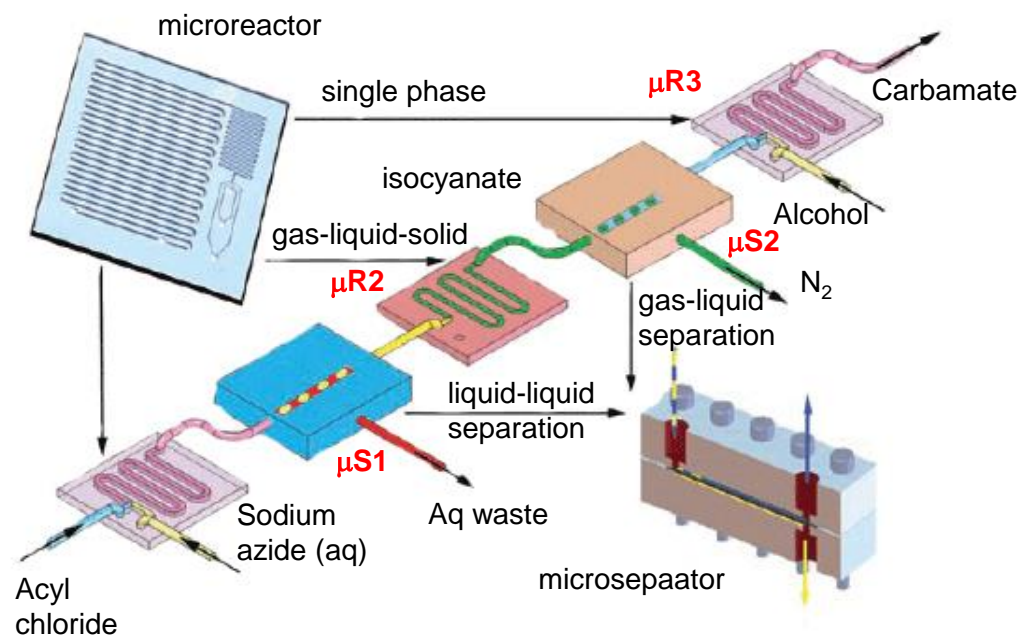
Paal-Knorr Synthesis via Microreactors.



FutureChemistry's FlowSyn on
Micronit Microfluidics microreactors

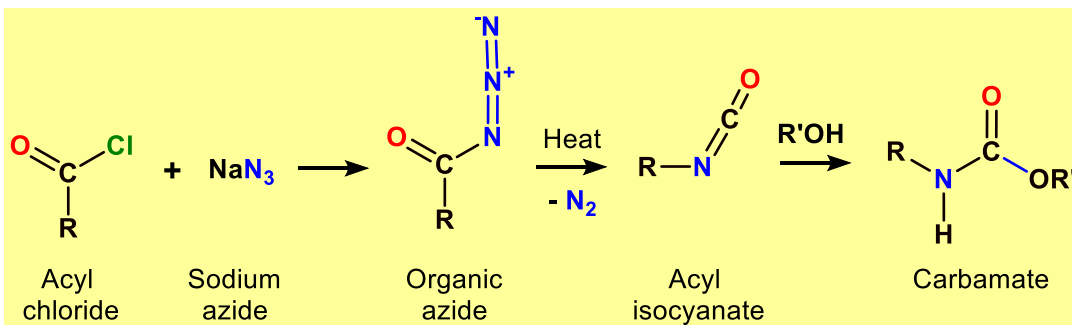


Miniaturization of Chemical Reaction: Synthesis of Carbamates.



Experimental setup for carbamate synthesis.

- μR₁, micro-reactor for conversion of acyl chloride to organic azide;
- μS₁, quantitative separation of organic and aqueous streams;
- μR₂, microreactor loaded with solid acid catalyst for conversion of organic azide to isocyanate;
- μS₂, quantitative separation of gaseous N₂ from the liquid;
- μR₃, microreactor for reaction of isocyanate and alcohol to carbamate.

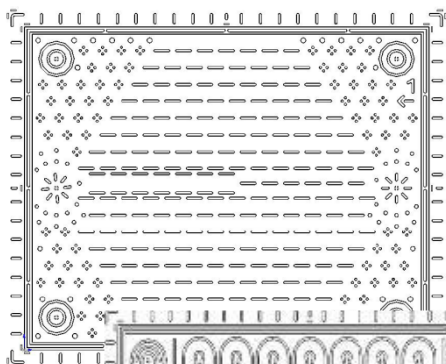


Hemantkumar R. Sahoo, Jason G. Kralj, and Klavs F. Jensen, *Angew. Chem.*, 2007, 46, 5704-5708.

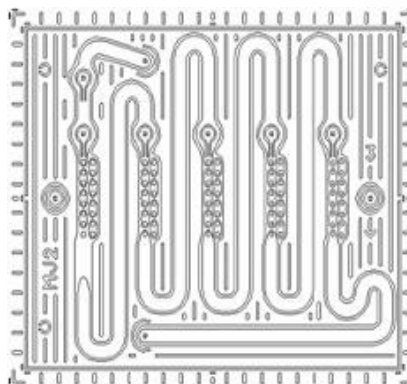
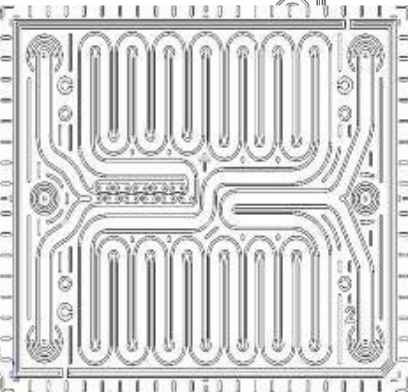
Sintesi di carbammati via azidi



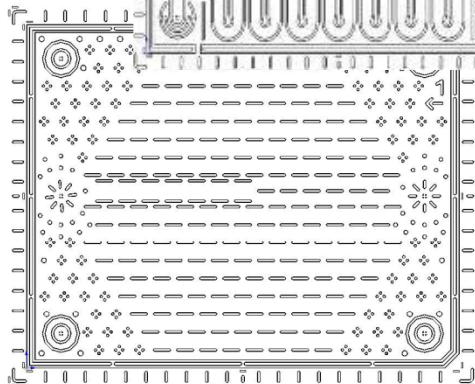
Corning Glass Microreactors.



Mixing
300 micron



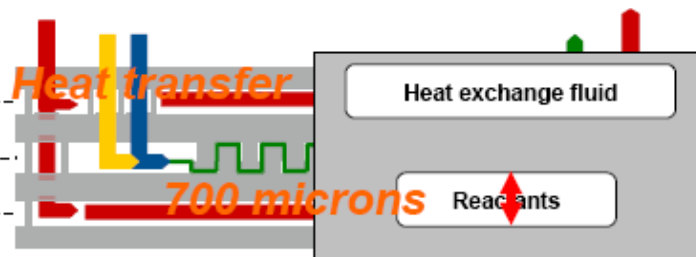
Pressure drop
1 millimeter



Heat exchange layer

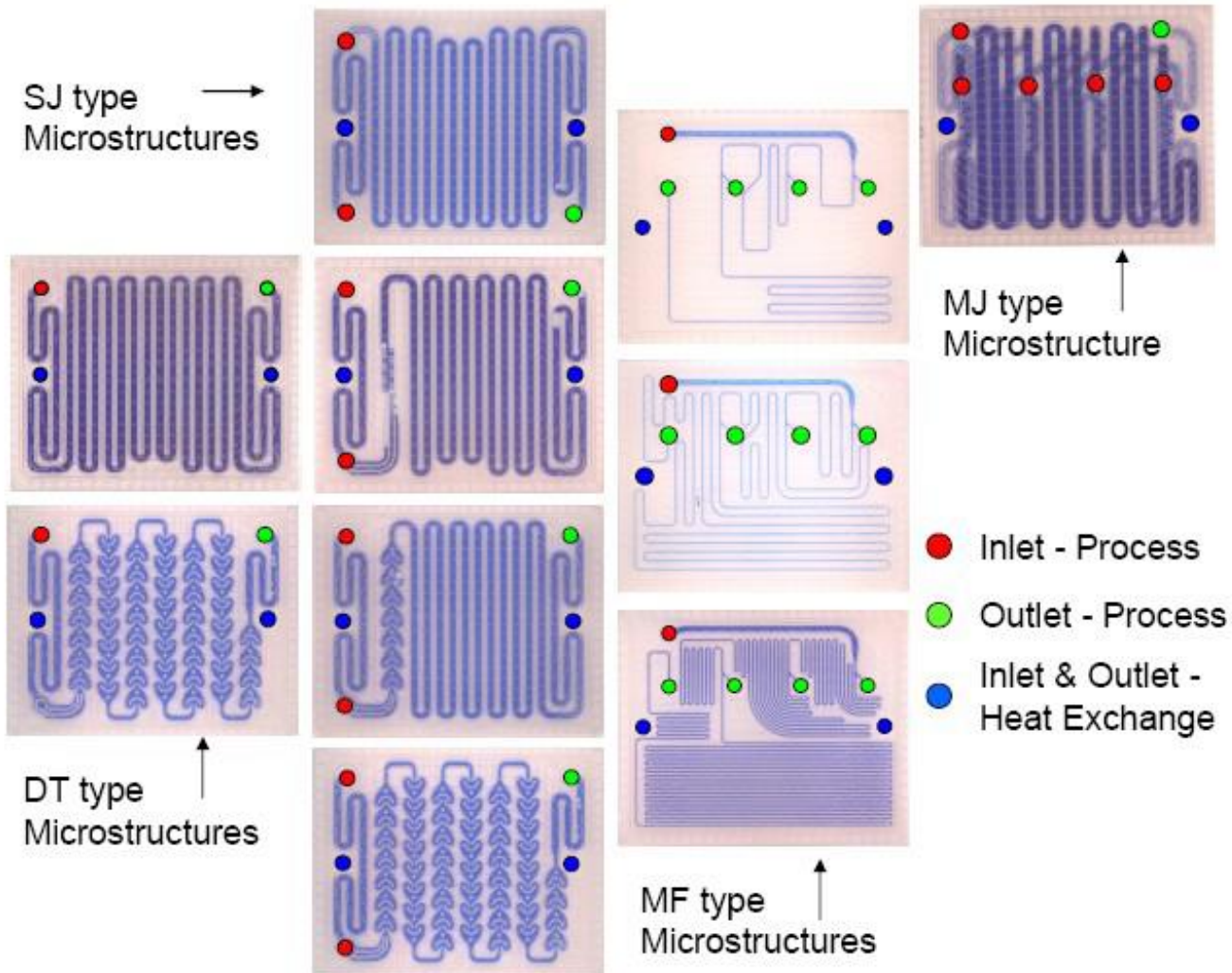
Reactants

Heat exchange layer





Fluidic Modules: Concept and Library.

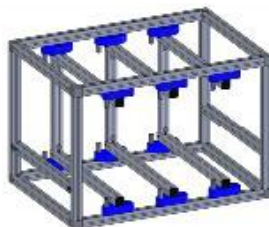




Engineered Reactor Components.



Interfaces



Frames



Standard Fittings



Connectors

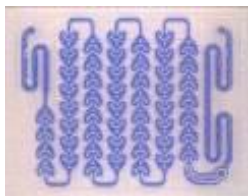


Tubing



O-ring seals

Sensors



Fluidic Modules

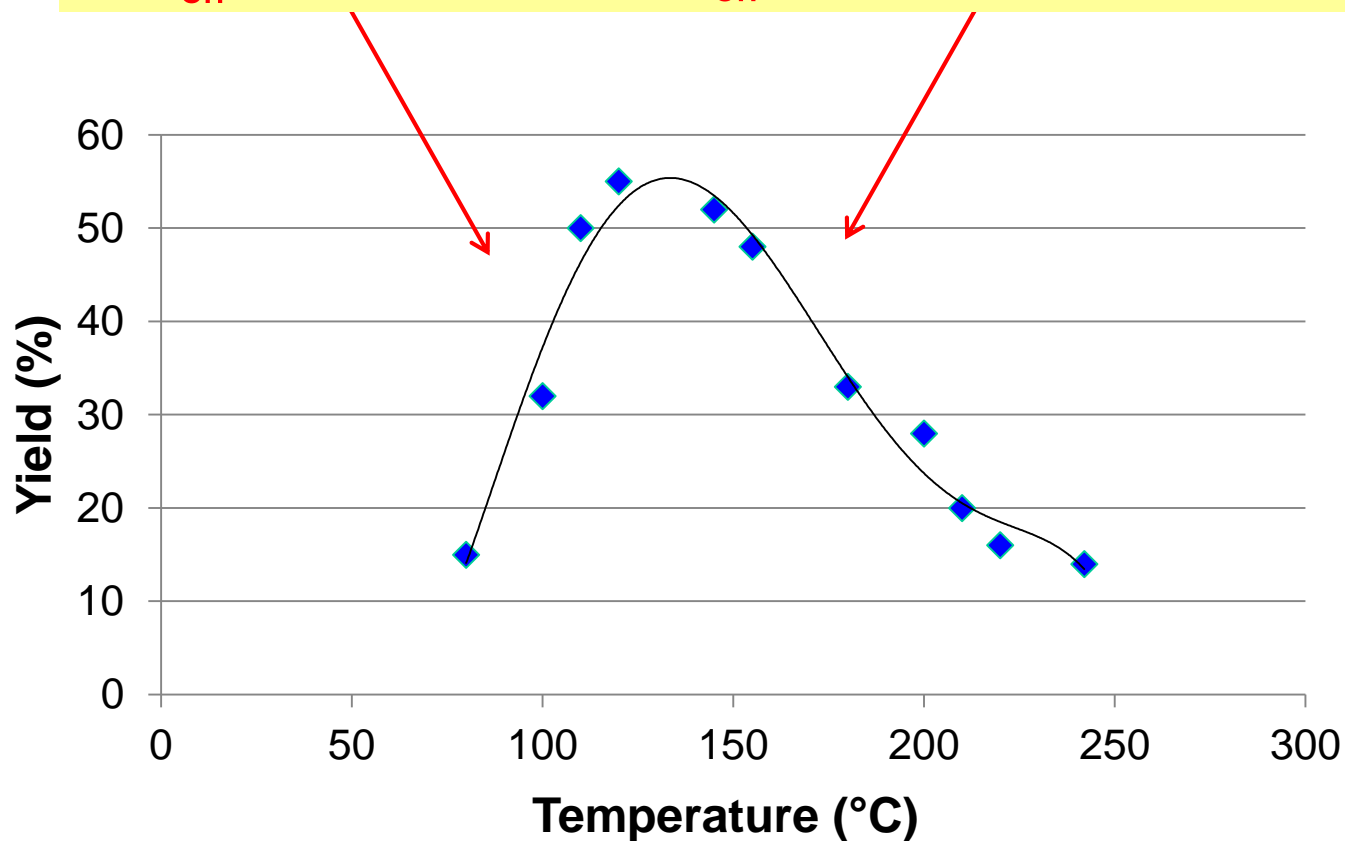
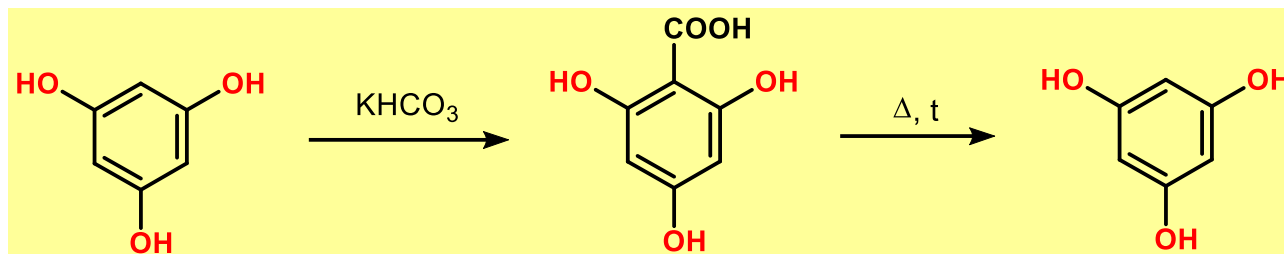
Instrumentation
(Pressure relief valve...)



Add-on
Labelling (insulation...)

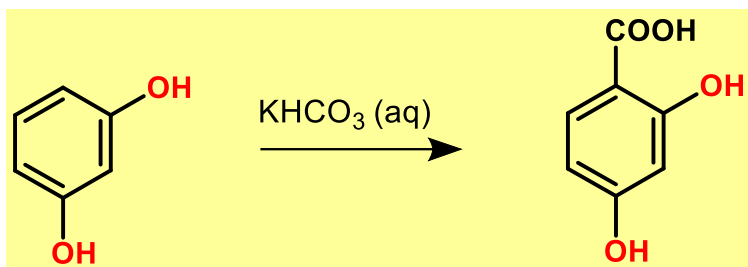


Phloroglucinol-Type Kolbe Schmitt - Synthesis in Microreactors.



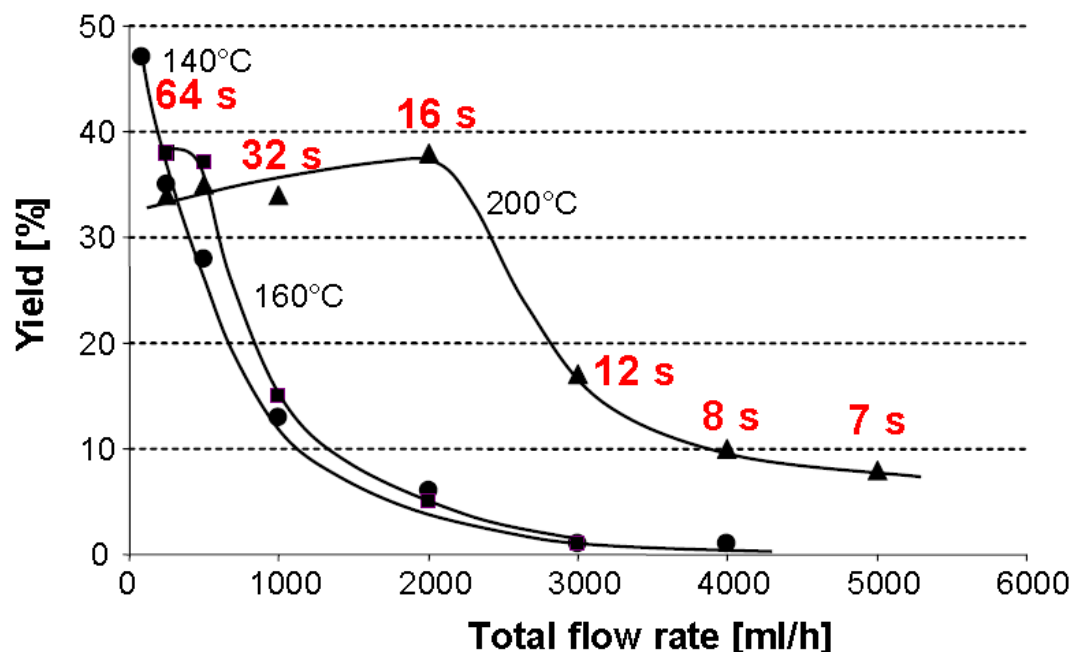


Kolbe Schmitt-Synthesis: High P,T-Processing.



V. Hessel, C. Hofmann, P. Löb, J. Löhndorf,
H. Löwe, A. Ziogas
Org.Proc. Res. Dev. **9**, 4(2005) 479-489

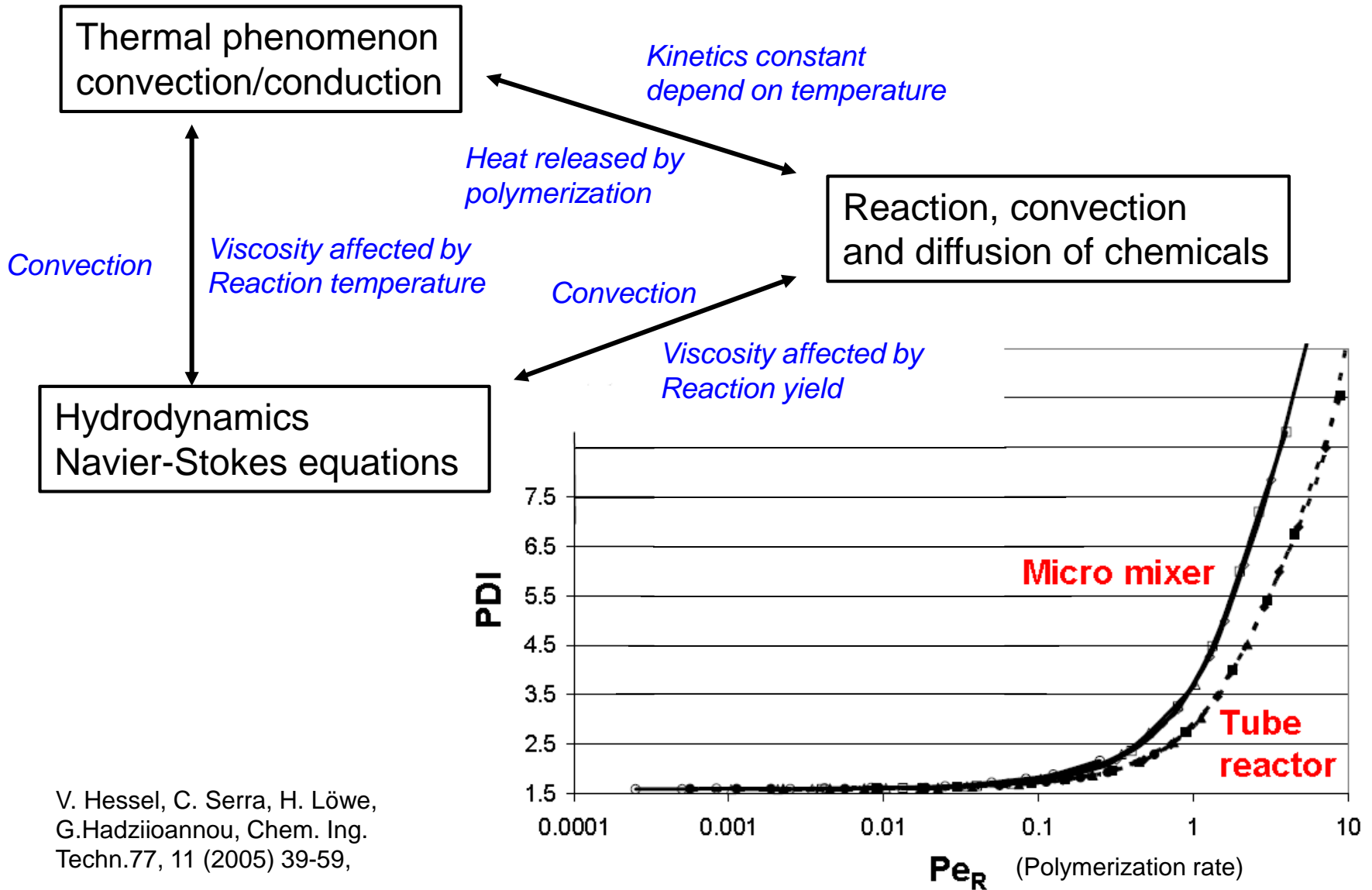
High p,T



- Pressure: 40-70 bar
 - Temperature: 100-220°C
 - Reaction time: 4 –390 s
- ⇒ Reduction of reaction time by ~2000
- ⇒ Increase in space-time yield by factor 440
- ⇒ Increase in productivity by factor 4



Modelling Study on Styrene Solution Polymerization.



V. Hessel, C. Serra, H. Löwe,
G. Hadziioannou, Chem. Ing.
Techn.77, 11 (2005) 39-59,

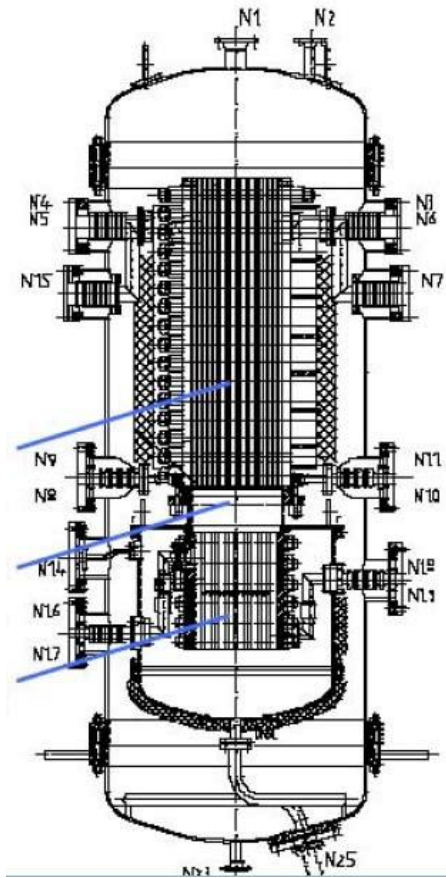


Microstructured Epoxidation Reactor.

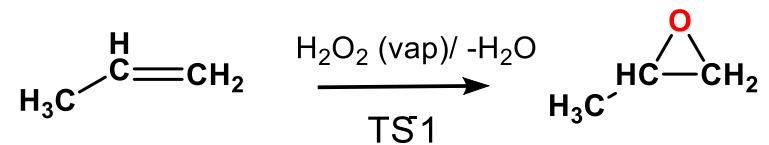


Reaction
(microstructured)
Mixing
(microstructured)
 H_2O_2 evaporation
(microstructured)

Degussa



Model Synthesis:

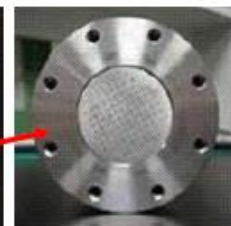


Features:

- Modular (unit operations, capacity)
- Multi-purpose (catalyst and reaction)
- Reaction under pressure
- Reactions in the explosive regime



Radical Polymerization Reactor.



Plant running at industrial site of Idemitsu Kosan

Dr. Takeshi Iwasaki (MCPT)
Proceedings IMRET 8, Atlanta, April 2005.



Where to Apply Microchemical Technology?

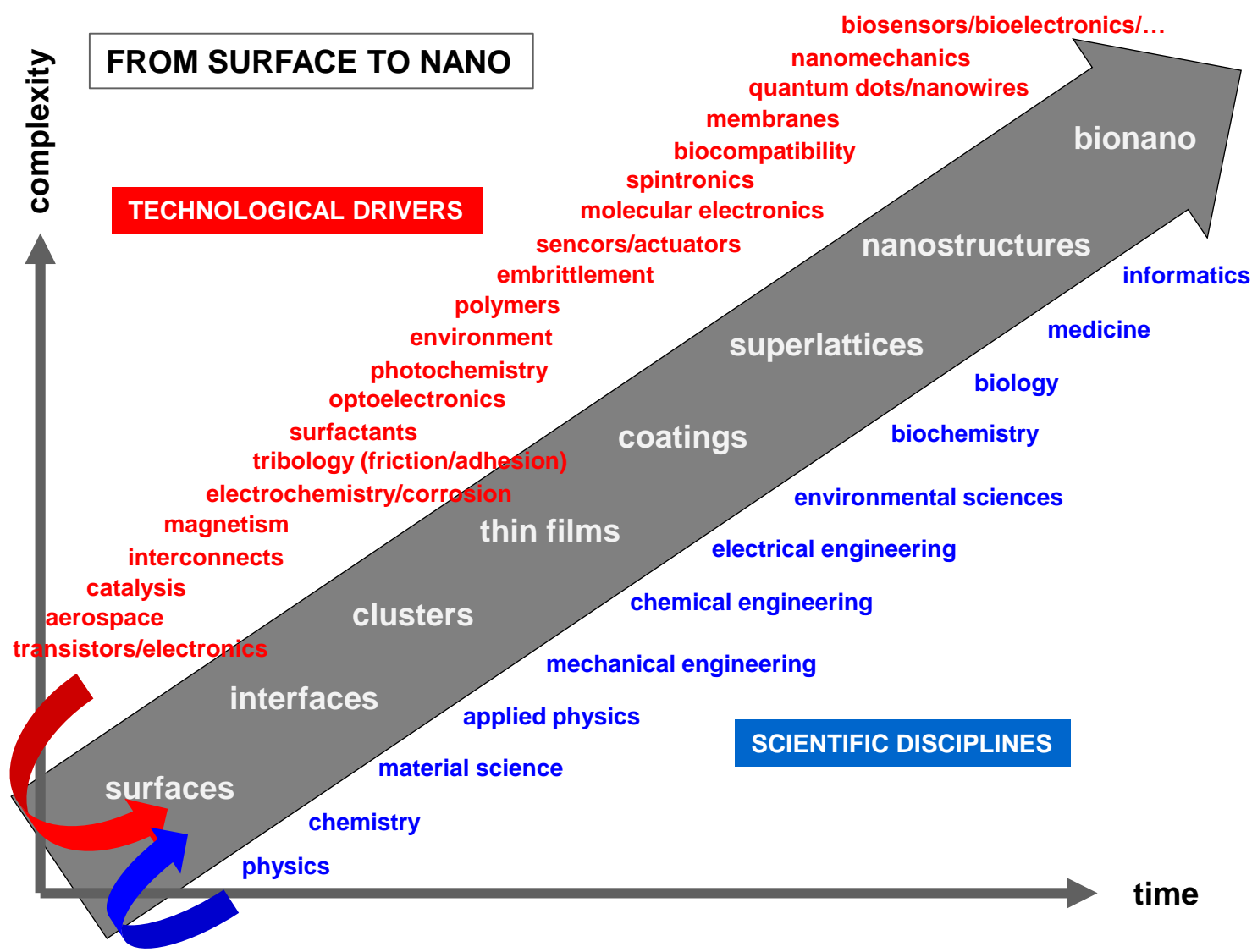
- Direct routes from hazardous systems
- Routes at increased concentration or even solvent-free
- Routes at elevated temperature and/or pressure
- Routes mixing the reactants 'all at once'
- Routes using unstable intermediates
- Routes in the explosive or thermal runaway regime
- Routes omitting the need of catalysts and auxiliary agents

DEVELOPMENT OF REACTORS TO ENABLE CHEMISTRY RATHER THAN SUBDUING CHEMISTRY AROUND THE REACTOR

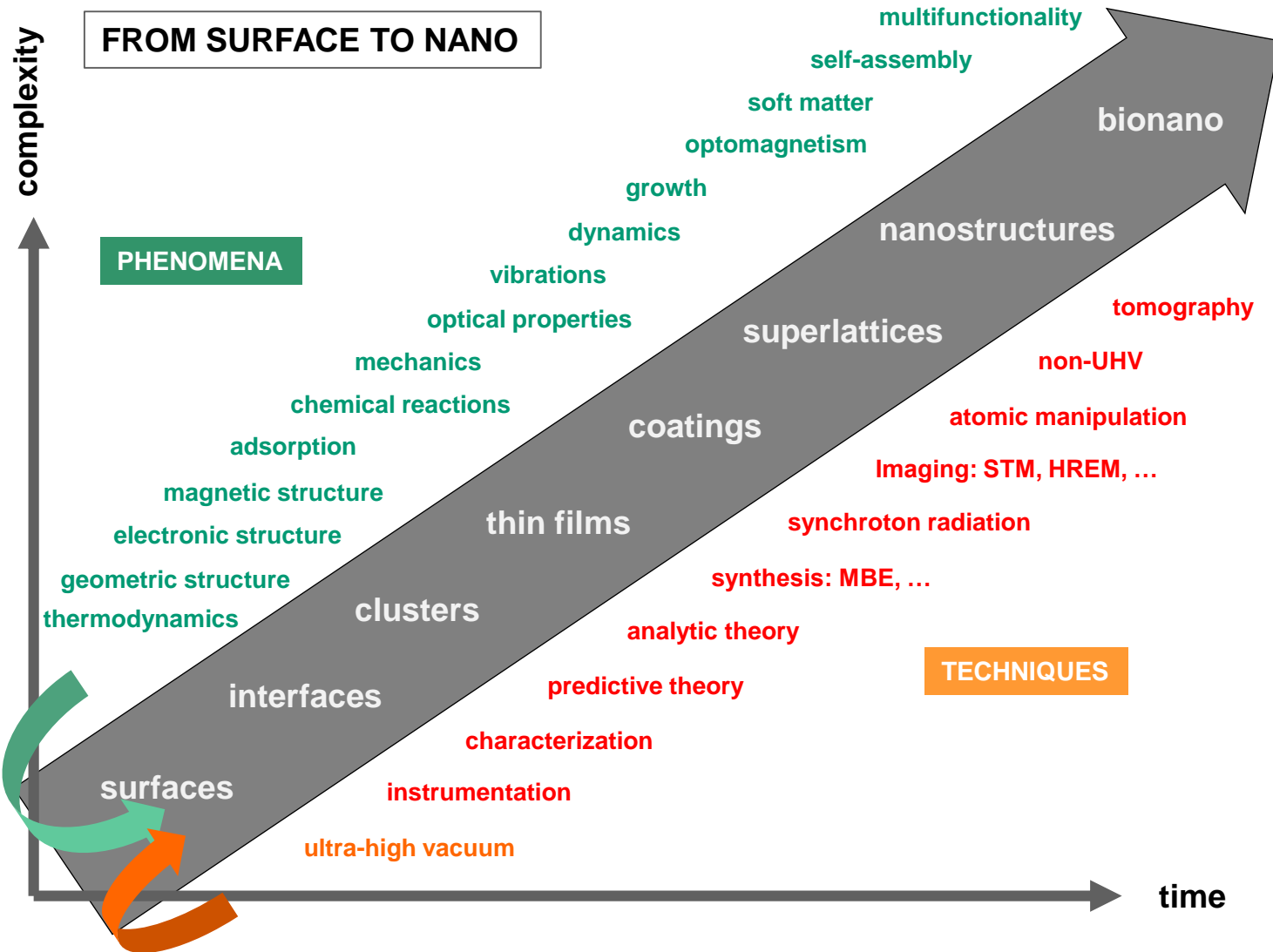
V. Hessel, P. Löb, H. Löwe, *Curr. Org. Chem.* 9, 8 (2005) 765-787
Jähnisch, K.; Hessel, V. et al.; *Angew. Chem. Intern. Ed.* 43, 4 (2004) 406-446



Scientific and Technological Drivers in Surface-Nano Applications.



Phenomena and Techniques in Surface-Nano Applications.





References on Microreactors and Microchemical Systems.

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2. Patrick L. Mills, David J. Quiram, James F. Ryley, Microreactor technology and process miniaturization for catalytic reactions—A perspective on recent developments and emerging technologies, Chemical Engineering Science, 2007, 62, 24, 6992
3. Paul Watts, Charlotte Wiles, Recent advances in synthetic micro reaction technology, Chem. Commun., 2007, 5, 443
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5. D. Ghislieri, K. Gilmore, P. H. Seeberger Control for divergent, continuous, multistep syntheses of active pharmaceutical ingredients" Angew. Chem., I.E. 2015, 54, 678–682
6. C. Y. Park, Y. J. Kim, H. J. Lim, J. H. Park, M. J. Kim, S. W. Seo, C. P. Park "Continuous flow photooxygenation of monoterpenes" RSC Advances 2015, 5, 4233–4237
7. Christoph Tonhauser, Adrian Natalello, Holger Löwe, Holger Frey, Microflow Technology in Polymer Synthesis, Macromolecules, 2012, 45, 24, 9551.
8. P. Wiktor, A. Brunner, P. Kahn, J. Qiu, M. Magee, X. F. Bian, K. Karthikeyan, J. LaBaer "Microreactor array device" Scientific Reports 2015, 5, Article number: 8736, doi: 10.1038/srep08736
9. Jun-ichi Yoshida, Heejin Kim, Aiichiro Nagaki, Green and Sustainable Chemical Synthesis Using Flow Microreactors, ChemSusChem, 2011, 4, 3, 331
10. Florence Bally, Christophe A. Serra, Volker Hessel, Georges Hadziioannou, Homogeneous Polymerization: Benefits Brought by Microprocess Technologies to the Synthesis and Production of Polymers, Macromolecular Reaction Engineering, 2010, 4, 9-10, 543
11. Jun Yue, Jaap C. Schouten, T. Alexander Nijhuis, Integration of Microreactors with Spectroscopic Detection for Online Reaction Monitoring and Catalyst Characterization, Industrial & Engineering Chemistry Research, 2012, 51, 45, 14583
12. Li-Hua Du, Xi-Ping Luo, Lipase-catalyzed regioselective acylation of sugar in microreactors, RSC Advances, 2012, 2, 7, 2663